

# 1 **Experimental study of potassium release during biomass-pellet combustion and** 2 **its interaction with inhibitive additives**

3 Yingzu Liu<sup>1</sup>, Kaidi Wan<sup>2,\*</sup>, Yong He<sup>1,\*</sup>, Zhihua Wang<sup>1</sup>, Jun Xia<sup>3</sup>, Kefa Cen<sup>1</sup>

4 1. State Key Laboratory of Clean Energy Utilization,  
5 Zhejiang University, Hangzhou 310027, China

6 2. CORIA – CNRS, Normandie Université,  
7 INSA de Rouen, 76800 Saint-Etienne-du-Rouvray, France

8 3. Department of Mechanical and Aerospace Engineering & Institute of Energy Futures,  
9 Brunel University London, Uxbridge UB8 3PH, UK

10 \* Corresponding authors: [kaidi.wan@coria.fr](mailto:kaidi.wan@coria.fr) (Kaidi Wan); [heyong@zju.edu.cn](mailto:heyong@zju.edu.cn) (Yong He).

## 12 **Abstract**

13 In the present study, two types of biomass were investigated as typical agricultural and woody  
14 biomass fuel, i.e., corn straw and poplar. Firstly, laser induced breakdown spectroscopy (LIBS) was  
15 employed to investigate the release characteristics of potassium (K) from a burning biomass pellet. In  
16 order to further investigate the correlation between K release and the combustion process, combustion  
17 parameters including pellet surface temperature and pellet diameter were simultaneously measured  
18 with LIBS. A dual-peak trend is observed in the K release history of poplar, but only a single peak is  
19 found in that of corn straw. Both biomass samples show the strongest K release during the  
20 devolatilization stage in comparison with the subsequent char burnout and ash cooking stages. Similar  
21 tendencies are observed between K release and pellet temperature, which suggests that K release is  
22 closely related to the combustion process. The K release mechanism can be attributed to temperature  
23 rise and therefore breakdown of chemical bonds during combustion. Then the release of different  
24 chemical forms of K was investigated by chemical fractionation treatment of the biomass samples.

25 The released amount of H<sub>2</sub>O-soluble, NH<sub>4</sub>Ac-soluble and HCl-soluble potassium compounds were  
26 obtained. The H<sub>2</sub>O-soluble potassium is found to be the major released potassium compound. Finally,  
27 four kinds of additives (two pure additives, i.e., silica and alumina, and two typical natural mineral  
28 additives, i.e., kaolin and mica) were added to the biomass samples to investigate their inhibition  
29 effects on K release. The natural sorbent additives show better inhibition effects than the pure ones.

30

31 *Keywords:* Potassium; LIBS; Fractionation; Inhibition; Biomass

32

### 33 **1. Introduction**

34 Biomass, as a renewable energy source, has been utilized to support 10–15% of the worldwide  
35 energy consumption [1], especially with soaring applications in thermal power production. However,  
36 advanced thermo-utilization of biomass is largely limited by severe ash deposition issues caused by  
37 alkali metal emissions [2]. Since potassium (K) is an important element for plants, it is usually rich in  
38 biomass. The potassium vapor released during the thermo-utilization of biomass tends to condense on  
39 cooler heat exchange surfaces and develop a sticky potassium layer. The sticky layer could capture fly  
40 ash and then result in ash deposition [3, 4]. Moreover, potassium could also react with sulfur and  
41 chlorine species, leading to severe fouling and corrosion [5, 6]. It is therefore important to understand  
42 potassium-release mechanisms during biomass combustion in order to develop potassium control  
43 technologies and achieve better utilization of biomass resources [7-10].

44 In the past few decades, experimental study on potassium release characteristics during biomass  
45 combustion has evolved from offline sampling approaches to online in-situ measurements using  
46 optical techniques [11-13]. These non-intrusive optical techniques can directly capture dynamic

47 potassium-release characteristics during biomass combustion. For instance, flame emission  
48 spectroscopy method has been employed to investigate potassium release characteristics [11] and the  
49 effects of different combustion atmosphere on potassium release [14] during biomass combustion.  
50 Weng et al. [15] measured the release of atomic potassium from burning coal, wood, and straw pellets  
51 using tunable diode laser absorption spectroscopy (TDLAS). Qu et al. [16] used the same technique to  
52 simultaneously measure the flame temperature, water vapor and atomic potassium distribution during  
53 entrained-flow biomass combustion and they observed that potassium species rapidly undergo primary  
54 ash transformation reactions even if the fuel particles reside in an oxygen-deficient environment. Other  
55 laser optical diagnostics techniques have also been used, including collinear photo-fragmentation  
56 atomic absorption spectroscopy (CPFAAS) [17], laser induced fragmentation fluorescence (ELIF) [18],  
57 laser-induced breakdown spectroscopy (LIBS) [19] and planar laser-induced fluorescence (PLIF) [20].  
58 In order to obtain the potassium proportion in solid residues, inductively coupled plasma-optical  
59 emission spectrometry (ICP-OES) is usually employed [21] to measure the remaining elemental  
60 potassium. Very recently, Liu et al. [22] used ICP-OES to investigate the effects of atmosphere and  
61 chlorine on potassium release during biomass combustion in a fluidized bed and the results show that  
62 the release proportion of potassium in air atmosphere was bigger than oxy-fuel environment and the  
63 overall activation energy for potassium release under air atmosphere is less than that under oxy-fuel  
64 atmosphere.

65 From previous studies [2, 23], we know that potassium compounds in biomass can be classified  
66 into four groups: (1) H<sub>2</sub>O-soluble potassium, which exists as potassium salts, e.g., potassium chloride;  
67 (2) CH<sub>3</sub>COONH<sub>4</sub> (NH<sub>4</sub>Ac)-soluble potassium, which is bounded to carboxyl groups; (3) HCl-soluble  
68 potassium, which is organically bounded to functional groups containing oxygen or nitrogen; (4)

69 insoluble potassium, which is attached to minerals.  $\text{NH}_4\text{Ac}$ - and  $\text{HCl}$ -soluble potassium compounds  
70 together are also referred to as organically-bound potassium. The release characteristics of individual  
71 forms of potassium compounds have been investigated mainly via offline inductively coupled plasma  
72 (ICP) measurements. For instance, Deng et al. [24] studied the transformation of different forms of  
73 potassium compounds during rapid pyrolysis of wheat straw, corn stalk and rice hull under different  
74 temperatures. On the other hand, numerical methods have also been utilized to investigate the release  
75 of different forms of potassium [25], e.g., the first order Arrhenius expression model [26], the two-step  
76 kinetics model [20] and even the two-step kinetics release model combined with the gas phase  
77 potassium transformation kinetics [27], although some key information such as the time-resolved  
78 release history of different forms of potassium are still lack for a complete model validation. To the  
79 authors' best knowledge, the online dynamic release characteristics of different forms of potassium  
80 compounds during biomass combustion have not been revealed yet.

81 To reduce harmful potassium emissions, inhibition technologies can be used and classified into  
82 the following two categories: (1) pretreatment by water washing to remove potassium before  
83 combustion [28] and (2) addition of potassium sorbent additives to inhibit potassium release during  
84 combustion [29]. While both approaches have shown their potential to alleviate ash deposition and  
85 corrosion in biomass-fired furnaces, the additive approach appears more advantageous in that it saves  
86 water and the additives can be directly injected into boilers without any major reconfiguration.  
87 Previous studies on inhibition additives of potassium release have shown that additives with a high  
88 content of Al or Si are effective to reduce potassium release [29, 30]. For example, Mason et al. [29]  
89 used flame emission method to investigated the effects of an aluminosilicate based additive on the  
90 release of potassium during biomass pellets combustion and the results suggest that high chlorine

91 and/or low (Si+Al) facilitates the release of KCl or KOH to the gas phase, while high (Si+Al) helps to  
92 keep K in the solid phase. To achieve a deeper understanding of the inhibition mechanism of various  
93 additives, however, the potassium-release dynamics that interacts with these additives during biomass  
94 combustion are still required.

95 In order to bridge these research gaps and achieve a better understanding of the release  
96 characteristics of different forms of potassium compounds and the inhibition mechanisms of different  
97 additives, the present study employs the LIBS technique to obtain time-resolved profiles of potassium  
98 released from a burning biomass pellet mixed with four different additives. In addition, offline ICP  
99 analyses are performed along with the chemical fractionation method to reveal the transformation of  
100 different chemical forms of potassium compounds in the solid phase. A combination of online and  
101 offline measurements can provide us comprehensive physical insights into potassium release during  
102 biomass combustion and its interaction with inhibitive additives.

103

## 104 **2. Experimental methods**

### 105 *2.1. Biomass samples and mineral additives*

106 Two biomass fuels, corn straw and poplar, have been used, which are representative agricultural  
107 and woody type biomass, respectively. The results of the proximate analysis, ultimate analysis and also  
108 the ash compositions of the two biomass samples are summarized in Table 1. The proximate analysis  
109 was determined via chemical analysis methods according to the Chinese National Standard GB/T 212-  
110 2008. The ultimate analysis was performed according to the Chinese National Standard GB/T 476-  
111 2008 (for carbon and hydrogen), GB/T 19227-2008 (for nitrogen) and GB/T 214-2007 (for sulfur).  
112 The mass fraction of oxygen was then calculated based on mass balance, i.e.,  $O_{daf}\% = 100\% - C_{daf}\%$

113 –  $H_{daf}\%$  –  $N_{daf}\%$  –  $S_{daf}\%$ . Ash compositions were obtained according to the Chinese National Standard  
 114 GB/T 1574-2007. One of the four additives was blended with the biomass samples to investigate their  
 115 inhibition effects on potassium release. Specifically, two pure additives, i.e., silica and alumina, and  
 116 two natural mineral additives, i.e., kaolin and mica, were employed. Table 2 gives the physical and  
 117 chemical properties of the four additives. All the additives were blended with the biomass at a dosing  
 118 ratio of 3% by weight, which is a typical dose for sorbents [31, 32]. To ensure the additives were well  
 119 mixed with the biomass, both the additives and biomass were first grounded and sieved to fine powder  
 120 with a diameter less than 75  $\mu\text{m}$ . Then they were mixed in a grinder of 32,000 rpm for 5 minutes to  
 121 obtain blended biomass-additive powders.

122

123 Table 1. Chemical analyses of biomass samples.

	Proximate analysis (wt.%)				Ultimate analysis (wt.%)						
	$M_{ad}$	$A_{ad}$	$V_{ad}$	$FC_{ad}$	$C_{daf}$	$H_{daf}$	$N_{daf}$	$S_{daf}$	$O_{daf}$		
Corn Straw	11.6±0.	7.9±0.1	64.2±1.	16.3±0.	43.9±0.	4.5±0.0	1.8±0.0	0.4±0.0	49.3±1.		
	22	2	27	42	94	9	6	9	03		
Poplar	11.6±0.	2.3±0.0	66.3±1.	19.8±0.	45.9±0.	4.1±0.0	0.7±0.0	0.1±0.0	49.2±1.		
	19	5	69	39	87	6	5	3	28		
Ash analysis (wt.%)								$Cl_{ad}$	$K_{ad}$	$P_{ad}$	
	SiO <sub>2</sub>	Al <sub>2</sub> O <sub>3</sub>	Fe <sub>2</sub> O <sub>3</sub>	CaO	MgO	K <sub>2</sub> O	Na <sub>2</sub> O		mg/g	mg/g	mg/g
Corn	47.52±	5.64±0	1.04±0	4.51±0	12.6±	7.87±0	1.97±0	Corn	1.34±0	13.1±0	0.7±0.
Straw	1.10	.29	.17	.38	0.72	.77	.14	Straw	.12	.79	11
Poplar	30.97±	5.09±0	2.6±0.	29.32±	5.96±	6.94±0	2.9±0.		1.04±0	7.09±0	
	0.89	.37	21	0.92	0.42	.85	17	Poplar	.11	.61	<0.1

124

125

126

Table 2. Physical and chemical properties of the additives.

	Silica	Alumina	Kaolin	Mica
<i>Dimensional parameter</i>				
Surface area (m <sup>2</sup> /g)	0.3	173	7.8	3.1
Pore volume (cm <sup>3</sup> /g)	0.002	0.244	0.037	0.012
Mean pore diameter (nm)	18.6	5.6	18.7	16.2
<i>Chemical composition (wt %)</i>				
Al <sub>2</sub> O <sub>3</sub>		>99	21.54±0.79	25.54±0.99
SiO <sub>2</sub>	>99		66.64±1.57	65.49±1.77
Na <sub>2</sub> O			0.18±0.01	0.73±0.04
CaO			0.12±0.01	0.18±0.02
MgO			0.43±0.02	2.06±0.19
Fe <sub>2</sub> O <sub>3</sub>			0.27±0.02	2.25±0.21
K <sub>2</sub> O			0.19±0.02	5.24±0.39

128

129 *2.2. Identification of the chemical forms of potassium*

130 Different chemical forms of potassium can be identified according to their solubility in different  
131 solvents through a chemical fractionation method. First, 1 gram of the biomass sample was added into  
132 100 ml water at 333 K, and the solution was stirred for 24 hours before a filtering operation is applied.  
133 The content of the H<sub>2</sub>O-soluble potassium such as potassium sulfates and chlorides can be determined  
134 by using inductively coupled plasmas-atomic emission spectroscopy (ICP-AES) to analyze the filtrate.  
135 The solid filter residue was then sequentially dissolved in 100 ml NH<sub>4</sub>Ac (1 mol/L) and 100 ml HCl  
136 (1 mol/L). The filtrate of each step was analyzed with ICP-AES to identify NH<sub>4</sub>Ac-soluble and HCl-  
137 soluble potassium. The final residual following HCl extraction was dissolved in strong acid and then  
138 analyzed with ICP-AES to determine the content of the insoluble potassium, such as potassium silicate.

139 The solid filter residuals obtained in each step, with H<sub>2</sub>O-soluble, NH<sub>4</sub>Ac-soluble, and HCl-

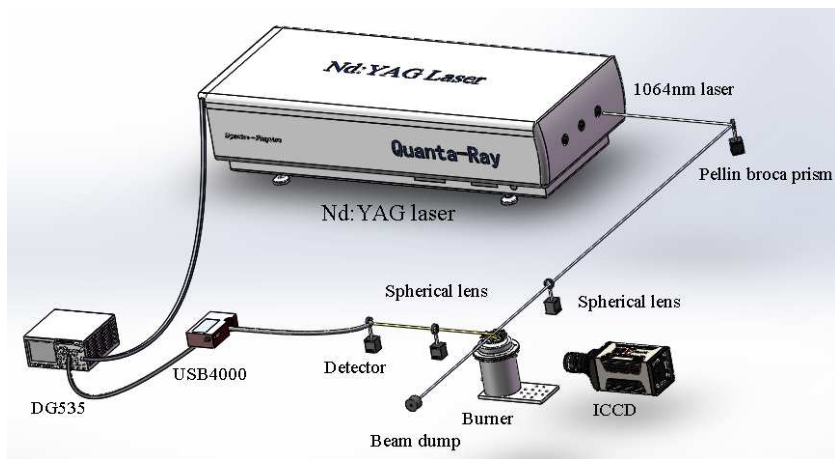
140 soluble potassium sequentially removed, were dried in an oven at 333 K for 24 h before further use.

141

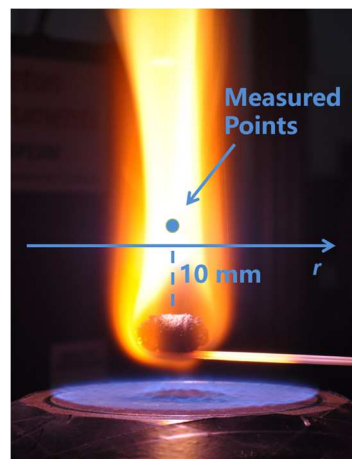
### 142 2.3. LIBS measurement system

143 The setup of the LIBS measurement system is shown in Fig. 1. A 4 mm spherical pellet was  
144 suspended on two ceramic rods (diameter of 1 mm) at a height of 10 mm above a heat flux burner. The  
145 pellet was produced by pressing 50 mg fuel powder, which are pulverized biomass, biomass-additive  
146 mixture or the solid filter residuals obtained in the chemical fractionation treatment. The maximum  
147 pressure used in the fabrication of the pellets could reach 2.5 MPa. The burner generated a laminar  
148 premixed methane-air flame at an equivalence ratio of 0.8. The flow rates of methane and air were  
149 0.59 SL/min and 7.06 SL/min, respectively. The flame was simulated using CHEMKIN with the GRI-  
150 3.0 mechanism [33]. The temperature at the pellet height was predicted to be 1892 K, and the major  
151 species compositions are 72.8% N<sub>2</sub>, 3.9% O<sub>2</sub>, 7.6% CO<sub>2</sub> and 15.4% H<sub>2</sub>O in mass.

152



(a) Configuration of equipment



(b) Measured location

153 Figure 1. LIBS measurement setup.

154

155 An Nd:YAG laser (Spectra Physics, model PRO-250) with a fundamental wavelength of 1064 nm  
156 was focused into the gas plume at 10 mm above the burning pellet. The repetition rate, pulse duration



157 and average energy of the laser were 10 Hz, 10 ns and 300 mJ, respectively. An Ocean Optics  
 158 spectrometer (model USB 4000) was employed to collect the LIBS signal. The laser and the  
 159 spectrometer were synchronized using a digital pulse generator (Stanford Research System, model  
 160 DG535).

161 To measure the quantitative potassium concentration, the LIBS signal was calibrated by  
 162 measuring the potassium spectral intensity (769.9 nm) for a potassium chloride (KCl) seeded flame of  
 163 a known concentration of potassium. The detailed calibration procedure can be found in our previous  
 164 study [34]. The obtained linear response of the LIBS signal to the potassium concentration is:

$$165 \quad I_{\text{LIBS,K}} = 1927C_{\text{K}}, R^2 = 0.97 \quad (1)$$

166 where  $I_{\text{LIBS,K}}$  is the LIBS signal intensity (-),  $C_{\text{K}}$  is the potassium concentration (mg/m<sup>3</sup>) at the  
 167 measuring point, and  $R^2$  is the coefficient of determination (-). The measurement uncertainties of the  
 168 LIBS system can be attributed to laser energy fluctuation, calibration uncertainty and electronic noise.  
 169 Base on the maximum error of calibration and measurement standard deviation, the maximal error  
 170 values of the K release rates are (a) Poplar:  $\pm 4.1 \times 10^{-4}$  mg/s ( $\pm 15.3\%$ ); (b) Corn Straw:  $\pm 1.8 \times 10^{-3}$  mg/s  
 171 ( $\pm 12.7\%$ ). The readers could refer to [20] for more detailed analyses on the experimental uncertainties.

172  
 173 *2.4. Optical measurement for the temperature and diameter of a pellet*

174 The surface temperature of a burning pellet was measured using a two-color pyrometer [35]. The  
 175 response of the two-color pyrometer,  $I_{(\lambda,T)}$ , is proportional to the radiant exitance of the measured pellet  
 176 surface [36]:

$$177 \quad I_{(\lambda,T)} = R_c \times S_\lambda \times \epsilon_\lambda \times \frac{C_1}{\lambda^5} \times e^{-C_2/(\lambda T)}, \quad (2)$$

178 where  $R_c$  is an instrument constant [37],  $S_\lambda$  is the spectral sensitivity of the charge coupled device

179 (CCD),  $\varepsilon_\lambda$  is the monochromatic emissivity,  $T$  is the pellet surface temperature (K), and  $C_1$  and  $C_2$  are  
 180 the first and second Planck's constants. By using Wien's equation to compare  $I_{(\lambda,T)}$  at two different  
 181 wavelengths, the pellet surface temperature can be calculated as [36]:

$$182 \quad T = \frac{C_2 \left( \frac{1}{\lambda_2} - \frac{1}{\lambda_1} \right)}{\ln \frac{I_{\lambda_1}}{I_{\lambda_2}} + \ln \frac{S_{\lambda_1}}{S_{\lambda_2}} + \ln \frac{\varepsilon_{\lambda_1}}{\varepsilon_{\lambda_2}} + \ln \frac{\lambda_1^5}{\lambda_2^5}} \quad . \quad (3)$$

183 The value of  $S_{\lambda_1}/S_{\lambda_2}$  was calibrated using a thermocouple in the flame produced by the heat flux burner,  
 184 for the purpose of correcting the spectral response of both the CCD and filters.

185 In the present study, a bioptic lens attachment (model LAVISION VZ-image doubler) is employed  
 186 to capture two-dimensional (2D) images of a pellet at 1 Hz. Two filters with a bandwidth of 1 nm,  
 187 which are centered at 633 nm and 647 nm, provide the spectral discrimination required for the two-  
 188 color pyrometry. Because the two wavelengths are close to each other,  $\varepsilon_{\lambda_1}/\varepsilon_{\lambda_2}$  is approximately unity.

189 The shape of a burning pellet can be obtained from the 2D images of thermal irradiation [38]. The  
 190 diameter of the pellet is then computed as the average of two orthogonal dimensions in each image.

191

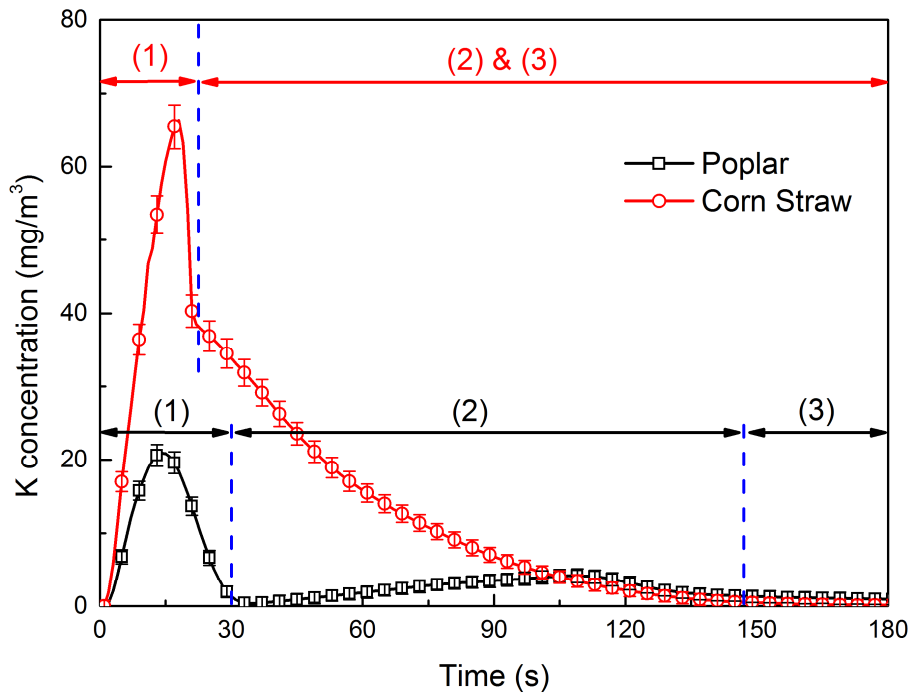
## 192 **3. Results and discussion**

### 193 *3.1. Potassium release characteristics of poplar and corn straw*

194 Temporal potassium release profiles of burning poplar and corn straw pellets measured by the  
 195 LIBS technique are shown in Fig. 2. Each measurement was repeated three times and the average result  
 196 is shown along with error bars indicating the statistical uncertainty of the measurements. A three-stage  
 197 release characteristics of potassium can be clearly observed for the poplar, which is similar to our  
 198 previous finding on the sodium release characteristics of a burning coal pellet [32, 39]: (1) the first  
 199 narrow peak appears during the devolatilization stage; (2) then a second wider peak occurs during the

200 char burnout stage; (3) finally, the potassium concentration slowly decreases to the baseline in the ash  
201 cooking stage. The three stages in Fig. 2 are separated according the method previously reported in  
202 [35]. For the corn straw, however, only one peak of the potassium concentration can be found in the  
203 devolatilization stage. Therefore, the second char burnout stage and the third ash cooking stage cannot  
204 be separated due to the lack of a second peak. Besides, the char burnout stage of corn straw features a  
205 monotonic decreasing profile of K concentration instead of a wide peak observed in that of poplar,  
206 which could be due to an overlap between the devolatilization and char burnout stages for corn straw.  
207 It indicates the char oxidation of the corn straw pellet proceeds in a different manner than that of poplar  
208 or coal combustion [20]. The kinetics and mechanism of char burnout may be different for poplar and  
209 corn straws due to their different fuel compositions and structures. From the ultimate analysis in Table  
210 1, the oxygen to carbon ratio is 1.123 for corn straw while 1.072 for poplar, which means poplar has a  
211 higher fuel rank than corn straw, i.e., poplar is closer to coal while corn straw is closer to agricultural  
212 biomass. As reported in [5], adding biomass to coal could leads the char burnout stage shifts towards  
213 an earlier time and get merged with the devolatilization stage.

214



215

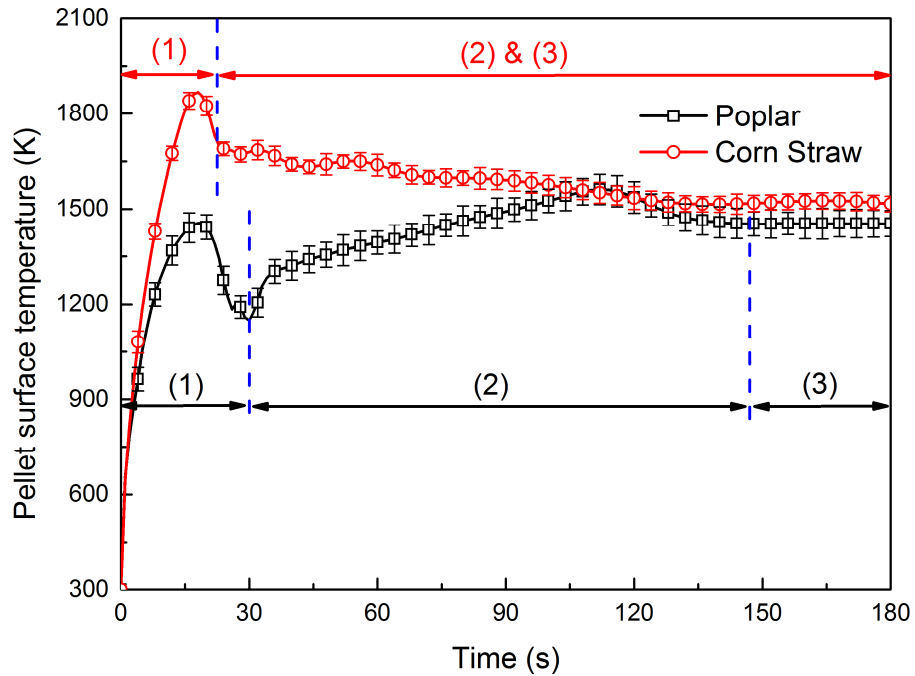
216 Figure 2. Temporal potassium release profiles of poplar and corn straw measured by LIBS. The three  
 217 combustion stages of the biomass pellets are: (1) devolatilization, (2) char burnout, and (3) ash  
 218 cooking.

219

220 Figure 3 shows temporal profiles of the surface temperature ( $T$ ) of the poplar and corn straw  
 221 pellets. Similar to the profiles of potassium release, the surface temperature profiles of the two biomass  
 222 samples are also different, with a dual-peak profile for poplar while a single-peak one for corn straw.  
 223 The dual-peak profile of poplar is similar to what has been observed in a burning coal pellet [39, 40]:  
 224 (1) in the first devolatilization stage, the pellet is rapidly heated by the high-temperature coflow and  
 225 volatile is released, leading to a volatile flame surrounding the pellet. The burning of volatile further  
 226 heats the pellet and leads to the first peak of the surface temperature; (2) since the heating effect of the  
 227 volatile flame disappears, the pellet slightly cools down. Then the thermal effect of char oxidation  
 228 heats the pellet again and results in the second peak of the surface temperature of poplar; (3) the  
 229 residual incombustible ash of the pellet achieves thermal equilibrium with the surrounding coflow. The  
 230 single-peak characteristic of corn straw is consistent with its potassium release profile, which suggests

231 a mild char oxidation as the pellet surface temperature gradually decreases towards the equilibrium  
232 temperature during the char and ash stages.

233

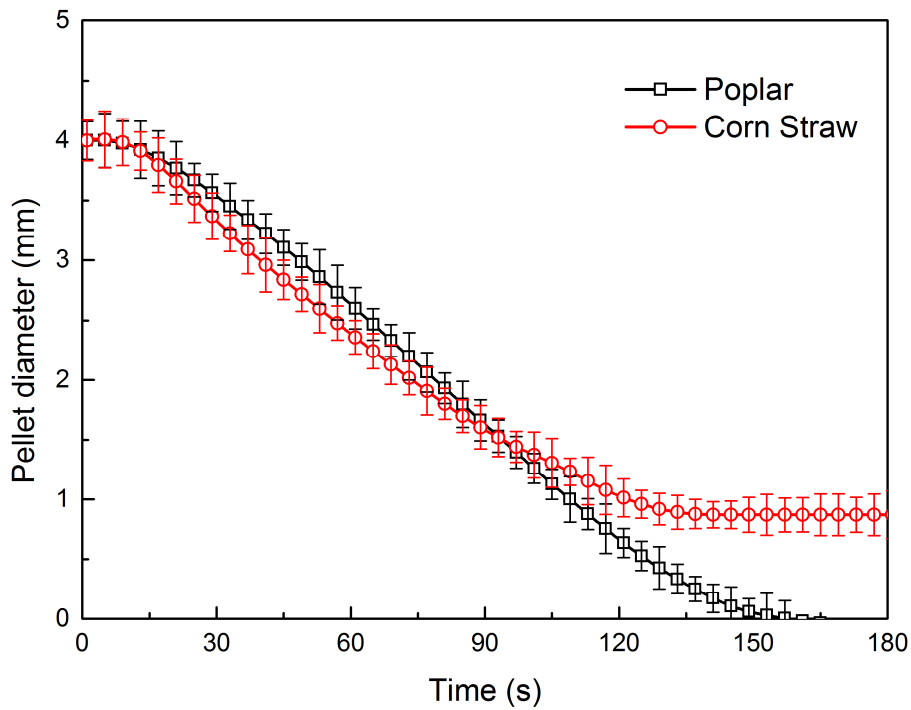


234

235 Figure 3. Temporal profiles of the surface temperature of poplar and corn straw pellets.

236

237 Figure 4 shows the temporal variation of the pellet diameter of poplar and corn straw during the  
238 combustion. It can be found the pellets experience a continuous and smooth shrinking process during  
239 all the three combustion stages. At the end of the experiments, the diameter of the corn straw pellet  
240 reduces to 0.87 mm, while that of the poplar pellet becomes too small to be measured. This is because  
241 poplar has an extremely low content of ash, i.e., only 2.3%.



242

243

Figure 4. Temporal profiles of the diameters of the poplar and corn straw pellets.

244

245

To further analyze the correlation between the potassium release, temperature and diameter of the

246

biomass pellets, the derivatives of the surface temperature and pellet diameter, i.e.,  $dT/dt$  and  $dD/dt$

247

are plotted in Fig. 5. The potassium concentration in the gas phase measured by LIBS in Fig. 2 can be

248

viewed as the derivative of the potassium content of the solid-fuel pellet. It can be observed that  $dT/dt$

249

experiences strong oscillations in the first 40 s for both poplar and corn straw during the highly active

250

devolatilization and early char-burning stages, and then it becomes smooth for the residual time period.

251

In contrast, the derivative of the pellet diameter  $dD/dt$  show a much smoother variation. It remains a

252

stable value around -0.03 during almost the whole char-burning stage of poplar from 30 s to 120 s,

253

which indicates the shrinking of the poplar pellet during the char burnout stage follows a linear trend.

254

For corn straw, the profile of  $dD/dt$  is a single- and wide-peak distribution, indicating the oxidization

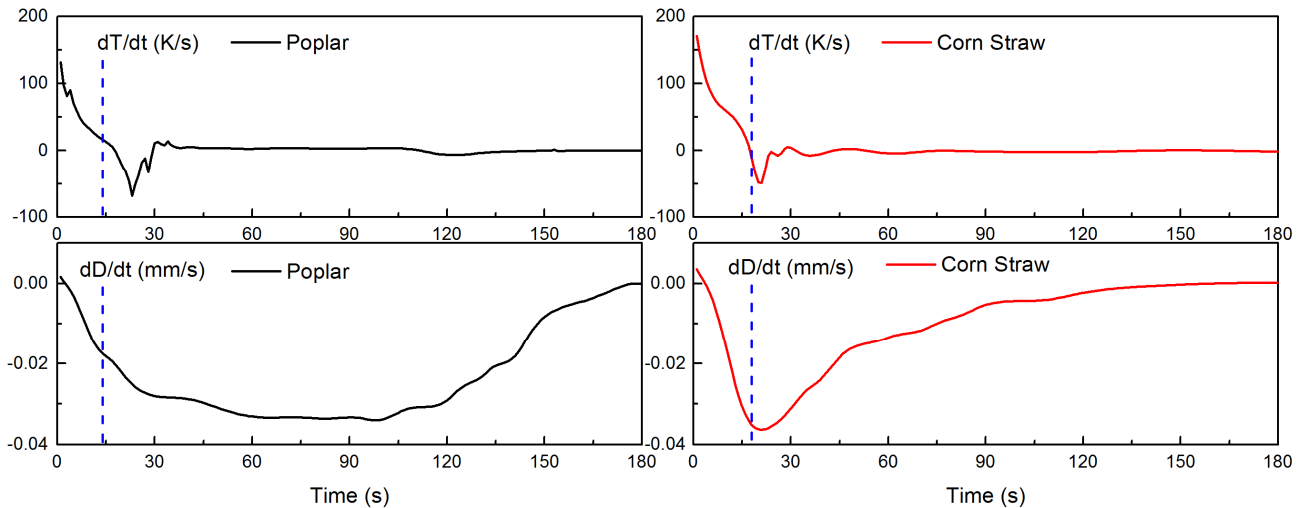
255

rate gradually decreases during the char-burning stage. The time corresponding to the maximum

256

potassium release rate is given by a dashed vertical line on the plots. It can be observed for both poplar

257 and corn straw,  $dT/dt$  changes from a positive to a negative value at this time, which indicates the  
 258 maximum pellet surface temperature is achieved. Since the devolatilization rate of biomass reaches its  
 259 maximum value at this time, the measured potassium concentration and the thermal effect of volatile  
 260 combustion both reach their peaks.  
 261



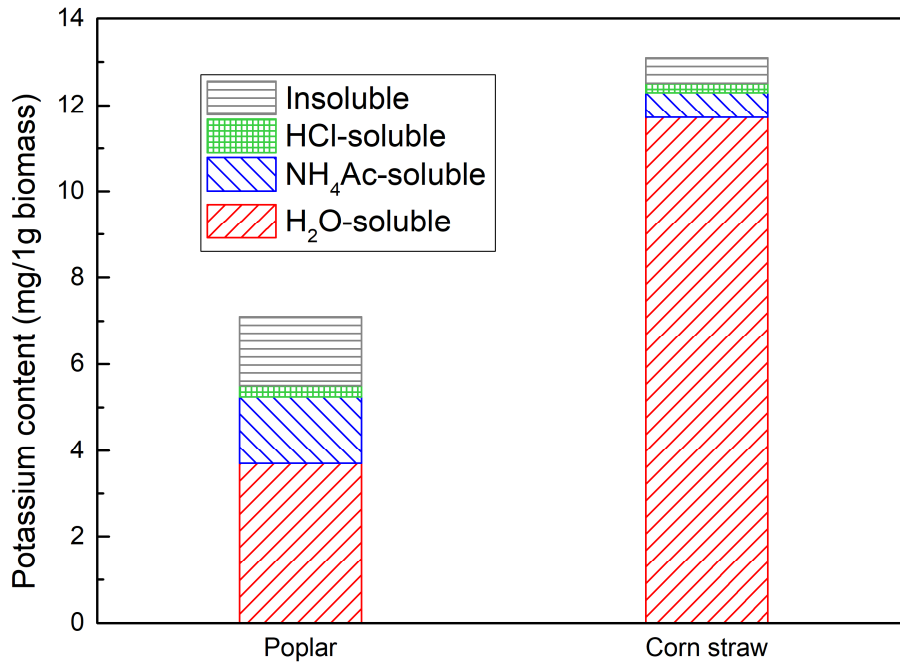
262  
 263 Figure 5. Temporal profiles of the derivatives of the surface temperature and diameter of the poplar  
 264 and corn straw pellets. The dashed vertical line illustrates the time when the maximum potassium  
 265 release rate is achieved.

### 267 3.2. Release characteristics of different chemical forms of potassium

268 Figure 6 shows the mass content of different chemical forms of potassium in poplar and corn  
 269 straw. The mass of different chemical forms of potassium (mg) in a biomass pellet sample prepared  
 270 from 1g of the raw poplar or corn straw was determined by performing ICP-AES on the filtrate  
 271 obtained from each step of the chemical extraction, as detailed in Section 2.2. It can be observed that  
 272 the major chemical form of potassium in both poplar and corn straw is H<sub>2</sub>O-soluble potassium, which  
 273 accounts for 52% and 90% of the total potassium mass in poplar and corn straw, respectively. The  
 274 HCl-soluble potassium is marginal, accounting for less than 4% of the total potassium mass in both

275 biomass samples. The residual potassium is evenly distributed in NH<sub>4</sub>Ac-soluble and insoluble forms  
276 for both poplar and corn straw.

277



278

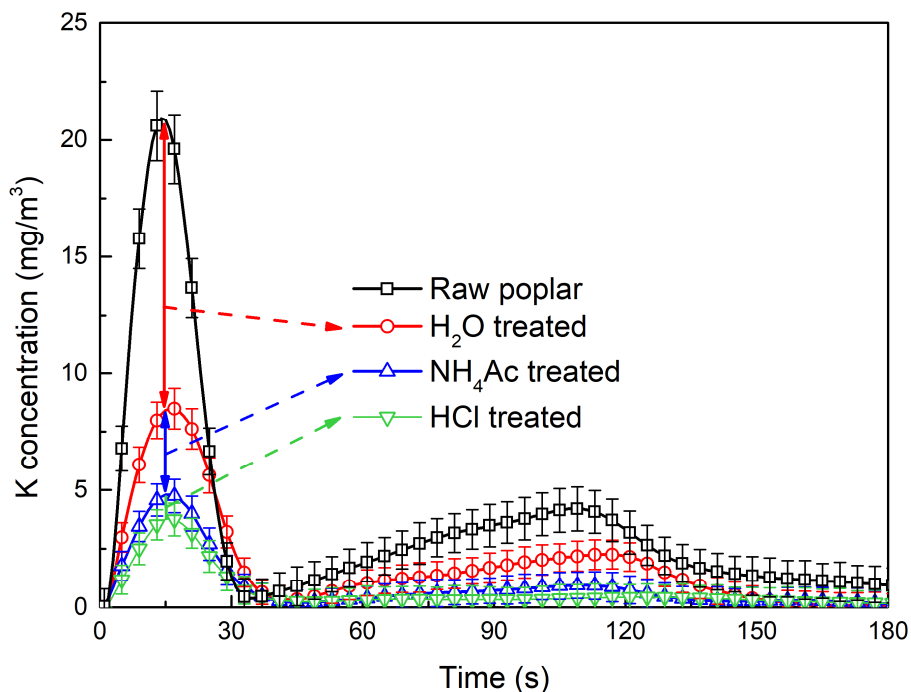
279 Figure 6. Content of different chemical forms of potassium in poplar and corn straw measured by  
280 ICP-AES.

281

282 Figure. 7 shows temporal potassium release profiles of pulverized poplar/corn straw pellets which  
283 were sequentially treated with H<sub>2</sub>O, NH<sub>4</sub>Ac and HCl. The difference between the potassium release  
284 profiles of the raw and H<sub>2</sub>O-treated biomass illustrates the contribution of H<sub>2</sub>O-soluble potassium in  
285 the total potassium release. Similarly, the contribution of NH<sub>4</sub>Ac-soluble and HCl-soluble potassium  
286 compounds can be obtained from the difference between other two adjacent profiles, as illustrated in  
287 Fig. 7. The profiles of HCl-treated biomass represent the release of insoluble potassium. Obviously,  
288 H<sub>2</sub>O-soluble potassium is the major potassium compound released during the combustion of the two  
289 biomass samples. After the biomass pellet is treated with H<sub>2</sub>O and therefore H<sub>2</sub>O-soluble potassium is  
290 removed, the potassium concentration detected by LIBS is largely decreased, especially for corn straw.

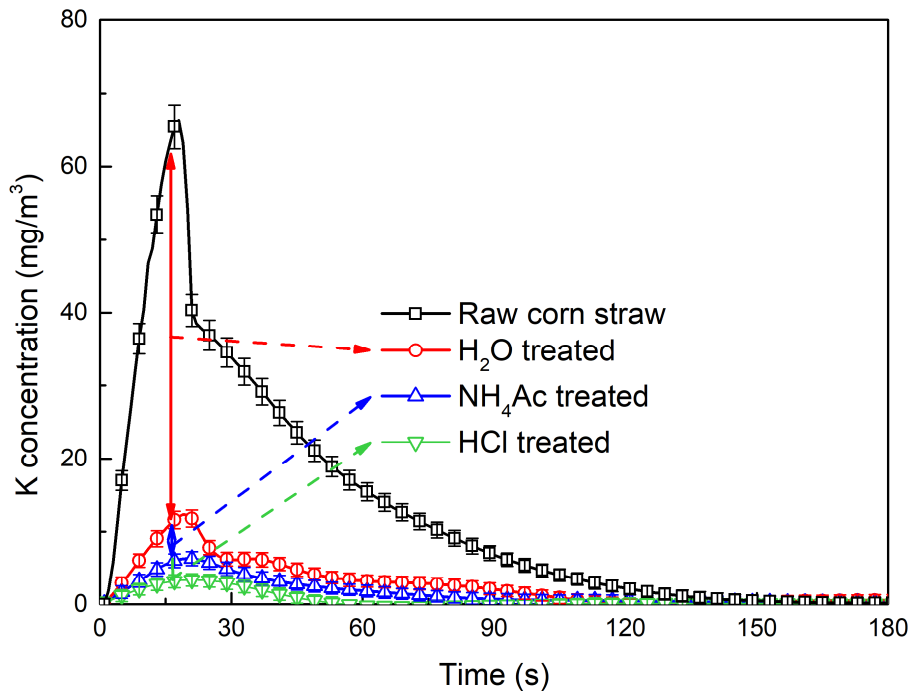


291 The removal of H<sub>2</sub>O-soluble potassium also affects the char burnout stage of poplar. As shown in Fig.  
292 7(a), the second peak of the H<sub>2</sub>O-treated profile is delayed compared to that of the raw poplar,  
293 indicating the combustion of the pellet slows down. This is similar to our previous findings on the  
294 sodium release of a burning coal pellet [39], which were attributed to catalytic effects of alkali metal  
295 on accelerating the combustion of char. The potassium release characteristics of H<sub>2</sub>O-, NH<sub>4</sub>Ac- and  
296 HCl-treated biomass follow a similar trend to that of the corresponding raw biomass, but with a lower  
297 magnitude of potassium concentration. Finally, insoluble potassium is found to be released mainly  
298 during the first devolatilization stage, which can be explained by the fact that insoluble-potassium  
299 micro-particles generated inside the porous structure of the biomass pellet will be transported outward  
300 by the volatile vapor generated during the devolatilization stage [41]. It should be noted that the  
301 chemical fractionation treatment could change the properties, e.g., porous structure, of the biomass  
302 samples, and therefore their combustion characteristics may be affected which in turn influence the  
303 potassium release characteristics.



305  
306

(a) Poplar



(b) Corn straw

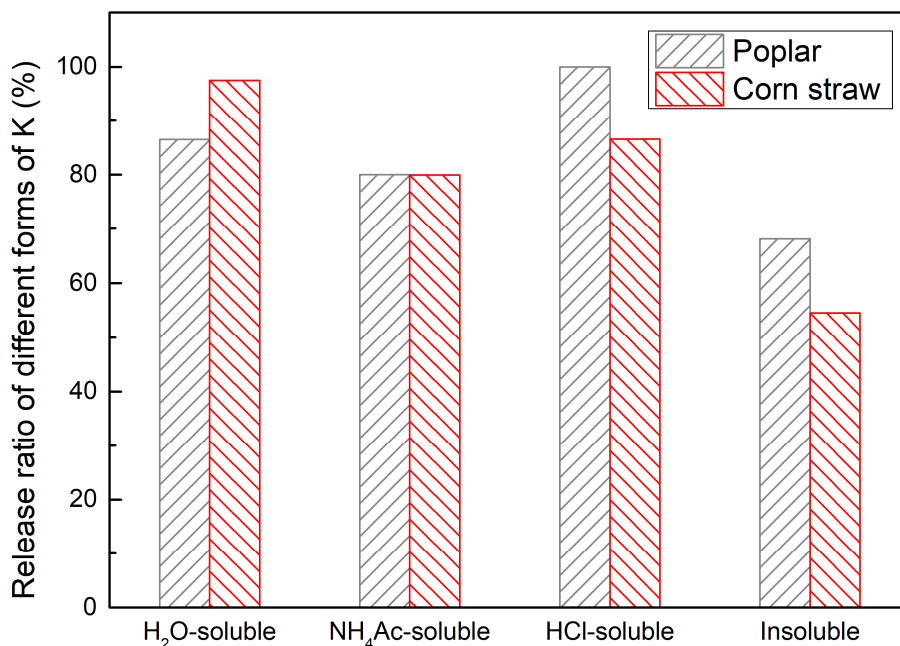
307

308

309 Figure 7. Temporal potassium release profiles of poplar and corn straw sequentially treated with  
 310 H<sub>2</sub>O, NH<sub>4</sub>Ac and HCl. The potassium release profiles of raw poplar and raw corn straw are also  
 311 presented as a reference.

312

313 Figure 8 summarizes the release ratio of different chemical forms of potassium during the  
 314 combustion of poplar and corn straw. ICP-AES was applied to the ashes of burned raw and H<sub>2</sub>O-,  
 315 NH<sub>4</sub>Ac- and HCl-treated biomass pellets to obtain the residual potassium mass in the ash. By  
 316 comparing it with the potassium mass in unburned raw and H<sub>2</sub>O-, NH<sub>4</sub>Ac- and HCl-treated biomass  
 317 pellets, the release ratio of different chemical forms of potassium can be determined. It can be observed  
 318 that the release ratio of H<sub>2</sub>O-, NH<sub>4</sub>Ac- and HCl-soluble potassium is relatively high, i.e., > 80% for  
 319 both poplar and corn straw; while that of insoluble potassium is lower and between 55–68%. The  
 320 release ratio reflects the release capability of different chemical forms of potassium. Specifically, H<sub>2</sub>O-,  
 321 NH<sub>4</sub>Ac- and HCl-soluble potassium compounds have a stronger release capability than insoluble  
 322 potassium during the combustion of the two biomass samples.



324

325 Figure 8. Release ratio of different chemical forms of potassium during the combustion of poplar and  
326 corn straw.

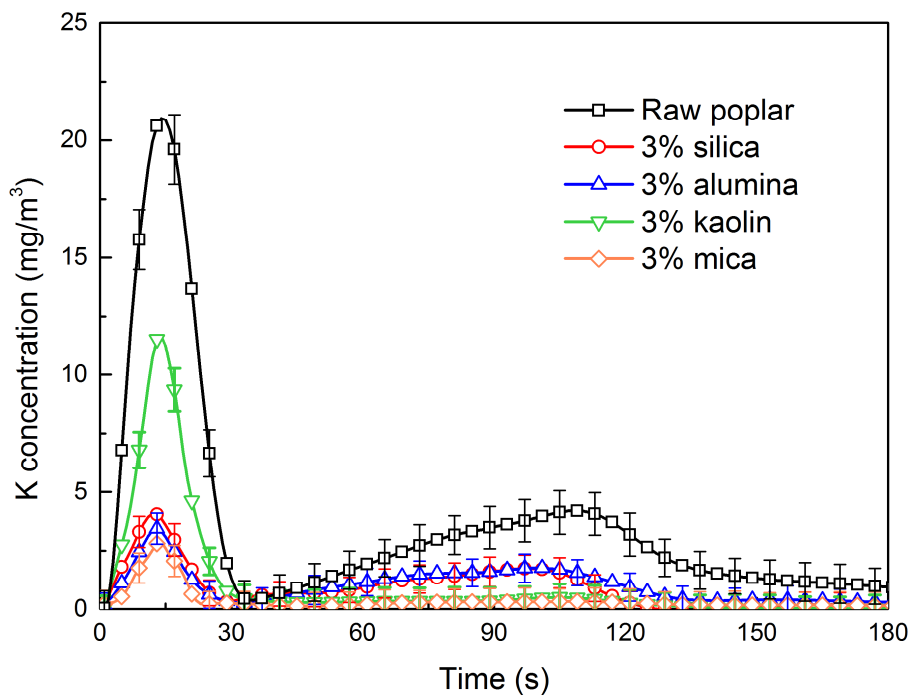
327

### 328 3.3. Inhibition effects of different additives on potassium release

329 A kind of additive was mixed with the biomass pellets of poplar and corn straw at a dosing ratio  
330 of 3% to investigate the inhibition effects of the additive on potassium release. Two pure additives, i.e.,  
331 silica and alumina, and two natural mineral additives, i.e., kaolin and mica, were used in the present  
332 study. Figure 9 shows the temporal potassium release profiles of poplar and corn straw pellets mixed  
333 with one of the four additives. Compared against the potassium release profiles of the raw biomass  
334 pellets, all the four additives are found to be able to significantly reduce the release of potassium during  
335 the combustion. Specifically, silica and alumina show a similar inhibition characteristic: the potassium  
336 release in the first devolatilization stage is largely prohibited, while the inhibition effect during the  
337 char burnout stage is moderate. For the natural mineral additives, kaolin shows a strong potassium  
338 inhibition capability during the char burnout and ash cooking stages, while its performance during the  
339 first devolatilization stage is not as good as the natural additives. Considering the potassium release

340 during the devolatilization stage is mainly due to the evaporation and thermal decomposition of  
341 inorganic potassium while in the char burnout stage the decomposition of organic potassium plays a  
342 dominate role [20], the above findings indicate that kaolin's retention effects on inorganic potassium  
343 are limited while silica and alumina have difficulties to retain organic potassium. Finally, mica shows  
344 the best potassium inhibition performance among the four additives during the entire process of  
345 biomass burning.

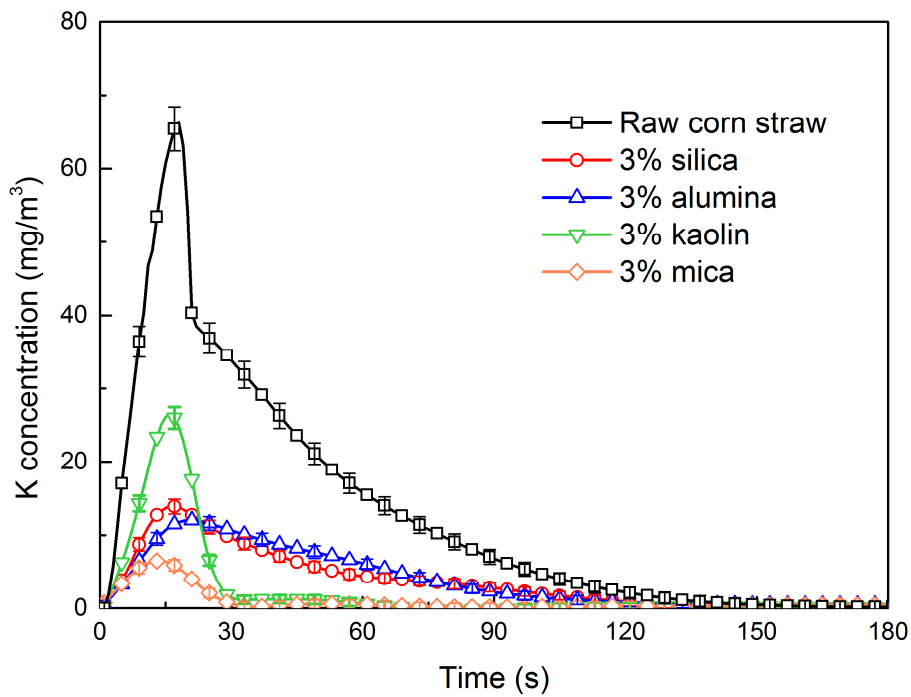
346



347

348

(a) Poplar



(b) Corn straw

Figure 9. Temporal potassium release profiles of raw biomass and biomass samples with 3% additives of silica, alumina, kaolin and mica.

349

350

351

352

353

354

355

356

357

358

359

360

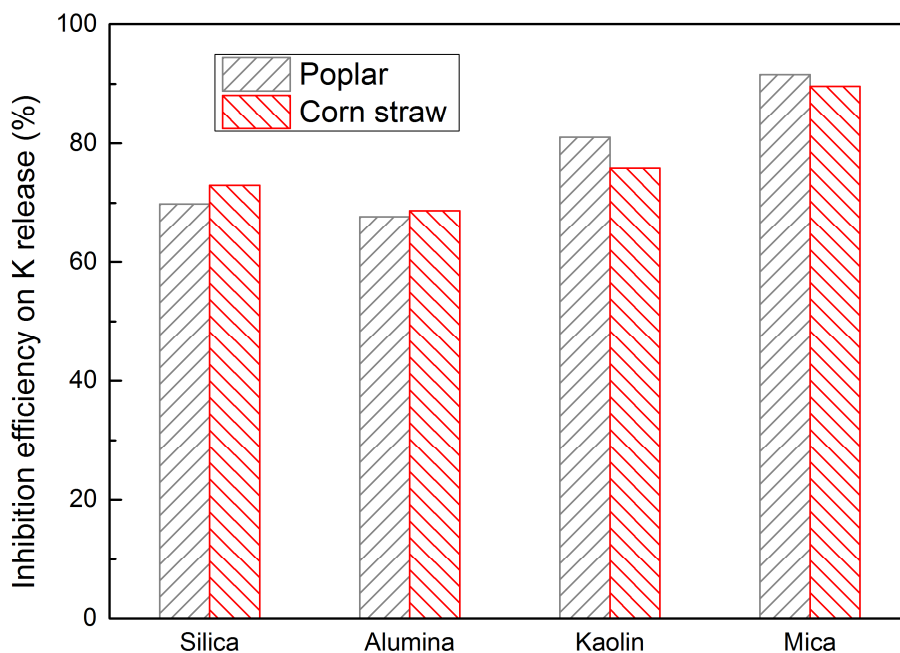
361

362

363

364

By performing ICP-AES to the ashes of those blended biomass-additives, the potassium release amount of each case can be calculated. Comparing these data with the potassium release amount of the raw biomass samples, the inhibition efficiency of the four additives on potassium release can then be obtained. As shown in Fig. 10, all the four additives achieve an inhibition efficiency higher than 65%, which indicates the additive approach can be an effective way to control potassium emissions during biomass combustion. The performance of the four additives on the two different types of biomass is consistent. The natural minerals have a better inhibition performance than the pure additives. Although kaolin's inhibition performance is the worst in the devolatilization stage, it achieves an overall higher inhibition efficiency than silica and alumina because the duration of the char burnout stage is much longer than the devolatilization stage. Mica is found to have the highest inhibition efficiency (90%) for both poplar and corn straw.



366

367 Figure 10. Efficiency of four additives, i.e., silica, alumina, kaolin and mica, on reducing potassium  
368 release during the combustion of poplar and corn straw.

369

#### 370 4. Conclusions

371 Potassium release and its interaction with inhibitive additives during the combustion of a  
372 poplar/corn straw pellet have been studied using a combination of online LIBS and offline ICP  
373 measurements. A dual-peak potassium release characteristic is observed for poplar while only a single  
374 peak is found for corn straw. The strongest potassium release is found in the first devolatilization stage  
375 for both biomass samples.

376 The release characteristics of different chemical forms of potassium are then measured by LIBS  
377 for the biomass samples sequentially treated with H<sub>2</sub>O, NH<sub>4</sub>Ac and HCl. H<sub>2</sub>O-soluble potassium is  
378 found to be the major released potassium compound. The corresponding ICP-AES analyses show that  
379 the release ratios of H<sub>2</sub>O-, NH<sub>4</sub>Ac- and HCl-soluble potassium are relatively high, i.e., > 80% for both  
380 poplar and corn straw; while that of insoluble potassium is lower and between 55–68%.

381 The inhibition effects of two pure additives, i.e., silica and alumina, and two natural mineral  
382 additives, i.e., kaolin and mica, on potassium release during biomass pellet combustion are studied.  
383 All the four additives achieve an inhibition efficiency higher than 65%, indicating the additive  
384 approach can be an effective way to control potassium emissions during biomass combustion. The  
385 natural minerals have a better inhibition performance than the pure additives, and mica is found to  
386 have the highest inhibition efficiency (90%) for both poplar and corn straw.

387

### 388 **Acknowledgements**

389 This work was jointly supported by the National Natural Science Foundation of China (51706200,  
390 51776185, 51706059), the China Postdoctoral Science Foundation (2019M650136, 2019TQ0277).  
391 Kaidi Wan would also like to acknowledge the support by the Centre national de la recherche  
392 scientifique (CNRS) of the France.

393

### 394 **References**

- 395 [1] Hosseini SE, Wahid MA. Utilization of palm solid residue as a source of renewable and sustainable  
396 energy in Malaysia. *Renewable and Sustainable Energy Reviews* 2014;40:621-32.
- 397 [2] Niu Y, Tan H, Hui Se. Ash-related issues during biomass combustion: Alkali-induced slagging,  
398 silicate melt-induced slagging (ash fusion), agglomeration, corrosion, ash utilization, and related  
399 countermeasures. *Prog. Energy Combust. Sci.* 2016;52:1-61.
- 400 [3] Liu Y, Cheng L, Zhao Y, Ji J, Wang Q, Luo Z, et al. Transformation behavior of alkali metals in  
401 high-alkali coals. *Fuel Process. Technol.* 2018;169:288-94.
- 402 [4] Capablo J. Formation of alkali salt deposits in biomass combustion. *Fuel Process. Technol.*  
403 2016;153:58-73.
- 404 [5] Liu YZ, He Y, Wang ZH, Xia J, Wan KD, Whiddon R, et al. Characteristics of alkali species release  
405 from a burning coal/biomass blend. *Appl. Energy* 2018;215:523-31.

- 406 [6] Fagerström J, Steinvall E, Boström D, Boman C. Alkali transformation during single pellet  
407 combustion of soft wood and wheat straw. *Fuel Process. Technol.* 2016;143:204-12.
- 408 [7] Paneru M, Babat S, Maier J, Scheffknecht G. Role of potassium in deposit formation during wood  
409 pellets combustion. *Fuel Process. Technol.* 2016;141:266-75.
- 410 [8] Capablo J, Ballester J. Experimental study of the kinetics of sulfation of alkali chloride deposits.  
411 *Fuel Process. Technol.* 2015;140:215-21.
- 412 [9] Ma T, Fan C, Hao L, Li S, Jensen PA, Song W, et al. Biomass ash induced agglomeration in  
413 fluidized bed. Part 2: Effect of potassium salts in different gas composition. *Fuel Process. Technol.*  
414 2018;180:130-9.
- 415 [10] Wan KD, Xia J, Vervisch L, Liu YZ, Wang ZH, Cen KF. Modelling alkali metal emissions in  
416 large-eddy simulation of a preheated pulverised-coal turbulent jet flame using tabulated chemistry.  
417 *Combust. Theory Model.* 2018;22(2):203-36.
- 418 [11] Mason PE, Jones JM, Darvell LI, Williams A. Gas phase potassium release from a single particle  
419 of biomass during high temperature combustion. *Proc. Combust. Inst.* 2017;36(2):2207-15.
- 420 [12] Mason PE, Darvell LI, Jones JM, Williams A. Observations on the release of gas-phase potassium  
421 during the combustion of single particles of biomass. *Fuel* 2016;182:110-7.
- 422 [13] Weng W, Costa M, Aldén M, Li Z. Single particle ignition and combustion of pulverized pine  
423 wood, wheat straw, rice husk and grape pomace. *Proc. Combust. Inst.* 2019;37(3):2663-71.
- 424 [14] He Z, Lou C, Fu J, Lim M. Experimental investigation on temporal release of potassium from  
425 biomass pellet combustion by flame emission spectroscopy. *Fuel* 2019;253:1378-84.
- 426 [15] Weng W, Gao Q, Wang Z, Whiddon R, He Y, Li Z, et al. Quantitative Measurement of Atomic  
427 Potassium in Plumes over Burning Solid Fuels Using Infrared-Diode Laser Spectroscopy. *Energy*  
428 *Fuels* 2017;31(3):2831-7.
- 429 [16] Qu Z, Holmgren P, Skoglund N, Wagner DR, Broström M, Schmidt FM. Distribution of  
430 temperature, H<sub>2</sub>O and atomic potassium during entrained flow biomass combustion – Coupling  
431 in situ TDLAS with modeling approaches and ash chemistry. *Combust. Flame* 2018;188:488-97.
- 432 [17] Sorvajärvi T, DeMartini N, Rossi J, Toivonen J. In Situ Measurement Technique for Simultaneous  
433 Detection of K, KCl, and KOH Vapors Released during Combustion of Solid Biomass Fuel in a  
434 Single Particle Reactor. *Appl. Spectrosc.* 2014;68(2):179-84.
- 435 [18] Erbel C, Mayerhofer M, Monkhouse P, Gaderer M, Spliethoff H. Continuous in situ measurements



436 of alkali species in the gasification of biomass. *Proc. Combust. Inst.* 2013;34(2):2331-8.

437 [19] Hsu L-J, Alwahabi ZT, Nathan GJ, Li Y, Li ZS, Aldén M. Sodium and Potassium Released from  
438 Burning Particles of Brown Coal and Pine Wood in a Laminar Premixed Methane Flame Using  
439 Quantitative Laser-Induced Breakdown Spectroscopy. *Appl. Spectrosc.* 2011;65(6):684-91.

440 [20] Liu YZ, Wang ZH, Xia J, Vervisch L, Wan KD, He Y, et al. Measurement and kinetics of elemental  
441 and atomic potassium release from a burning biomass pellet. *Proc. Combust. Inst.*  
442 2019;37(3):2681-8.

443 [21] Tchoffor PA, Moradian F, Pettersson A, Davidsson KO, Thunman H. Influence of Fuel Ash  
444 Characteristics on the Release of Potassium, Chlorine, and Sulfur from Biomass Fuels under  
445 Steam-Fluidized Bed Gasification Conditions. *Energy Fuels* 2016;30(12):10435-42.

446 [22] Zhang Z, Liu J, Shen F, Dong Y. Insights into the Effects of Atmosphere and Chlorine on  
447 Potassium Release during Biomass Combustion: Temporal Measurement and Kinetic Studies.  
448 *Energy Fuels* 2018;32(12):12523-31.

449 [23] Wan K, Wang Z, Xia J, Vervisch L, Domingo P, Lv Y, et al. Numerical study of HCl and SO<sub>2</sub>  
450 impact on sodium emissions in pulverized-coal flames. *Fuel* 2019;250:315-26.

451 [24] Deng L, Ye J, Jin X, Che D. Transformation and release of potassium during fixed-bed pyrolysis  
452 of biomass. *Journal of the Energy Institute* 2018;91(4):630-7.

453 [25] Wan KD, Wang ZH, Xia J, Vervisch L, Domingo P, Lv Y, et al. Numerical study of HCl and SO<sub>2</sub>  
454 impact on potassium emissions in pulverized-biomass combustion. *Fuel Process. Technol.*  
455 2019;193:19-30.

456 [26] Fatehi H, Li ZS, Bai XS, Aldén M. Modeling of alkali metal release during biomass pyrolysis.  
457 *Proc. Combust. Inst.* 2017;36(2):2243-51.

458 [27] Cao W, Martí-Rosselló T, Li J, Lue L. Prediction of potassium compounds released from biomass  
459 during combustion. *Appl. Energy* 2019;250:1696-705.

460 [28] Deng L, Zhang T, Che D. Effect of water washing on fuel properties, pyrolysis and combustion  
461 characteristics, and ash fusibility of biomass. *Fuel Process. Technol.* 2013;106:712-20.

462 [29] Clery DS, Mason PE, Rayner CM, Jones JM. The effects of an additive on the release of potassium  
463 in biomass combustion. *Fuel* 2018;214:647-55.

464 [30] Steenari BM, Karlfeldt Fedje K. Addition of kaolin as potassium sorbent in the combustion of  
465 wood fuel – Effects on fly ash properties. *Fuel* 2010;89(8):2026-32.

- 466 [31] He Y, Whiddon R, Wang ZH, Liu YZ, Zhu YQ, Liu JZ, et al. Inhibition of Sodium Release from  
467 Zhundong Coal via the Addition of Mineral Additives: Online Combustion Measurement with  
468 Laser-Induced Breakdown Spectroscopy (LIBS). *Energy Fuels* 2017;31(2):1082-90.
- 469 [32] Liu YZ, Wang ZH, Lv Y, Wan KD, He Y, Xia J, et al. Inhibition of sodium release from Zhundong  
470 coal via the addition of mineral additives: A combination of online multi-point LIBS and offline  
471 experimental measurements. *Fuel* 2018;212:498-505.
- 472 [33] Smith GP, Golden DM, Frenklach M, Moriarty NW, Eiteneer B, Goldenberg M, et al. GRI-Mech  
473 3.0. ([http://www.me.berkeley.edu/gri\\_mech/](http://www.me.berkeley.edu/gri_mech/)).
- 474 [34] He Y, Zhu JJ, Li B, Wang ZH, Li ZS, Aldén M, et al. In-situ measurement of sodium and potassium  
475 release during oxy-fuel combustion of lignite using laser-induced breakdown spectroscopy:  
476 effects of O<sub>2</sub> and CO<sub>2</sub> concentration. *Energy Fuels* 2013;27(2):1123-30.
- 477 [35] Liu YZ, He Y, Wang ZH, Wan KD, Xia J, Liu JZ, et al. Multi-point LIBS measurement and  
478 kinetics modeling of sodium release from a burning Zhundong coal particle. *Combust. Flame*  
479 2018;189:77-86.
- 480 [36] Huang Y, Yan Y, Riley G. Vision-based measurement of temperature distribution in a 500-kW  
481 model furnace using the two-colour method. *Measurement* 2000;28(3):175-83.
- 482 [37] DeWitt DP, Nutter GD. *Theory and practice of radiation thermometry*. Wiley Online Library; 1988.
- 483 [38] van Eyk PJ, Ashman PJ, Alwahabi ZT, Nathan GJ. Simultaneous measurements of the release of  
484 atomic sodium, particle diameter and particle temperature for a single burning coal particle. *Proc.*  
485 *Combust. Inst.* 2009;32(2):2099-106.
- 486 [39] Liu YZ, Wang ZH, Wan KD, Lv Y, Xia J, He Y, et al. In Situ Measurements of the Release  
487 Characteristics and Catalytic Effects of Different Chemical Forms of Sodium during Combustion  
488 of Zhundong Coal. *Energy Fuels* 2018;32(6):6595-602.
- 489 [40] Wang ZH, Liu YZ, Whiddon R, Wan KD, He Y, Xia J, et al. Measurement of atomic sodium  
490 release during pyrolysis and combustion of sodium-enriched Zhundong coal pellet. *Combust.*  
491 *Flame* 2017;176:429-38.
- 492 [41] Wan KD, Vervisch L, Xia J, Domingo P, Wang ZH, Liu YZ, et al. Alkali metal emissions in an  
493 early-stage pulverized-coal flame: DNS analysis of reacting layers and chemistry tabulation. *Proc.*  
494 *Combust. Inst.* 2019;37(3):2791-9.

495

## Figure captions

Figure 1. LIBS measurement setup.

Figure 2. Temporal potassium release profiles of poplar and corn straw measured by LIBS. The three combustion stages of the biomass pellets are: (1) devolatilization, (2) char burnout, and (3) ash cooking.

Figure 3. Temporal profiles of the surface temperature of poplar and corn straw pellets.

Figure 4. Temporal profiles of the diameters of the poplar and corn straw pellets.

Figure 5. Temporal profiles of the derivatives of the surface temperature and diameter of the poplar and corn straw pellets. The dashed vertical line illustrates the time when the maximum potassium release rate is achieved.

Figure 6. Content of different chemical forms of potassium in poplar and corn straw measured by ICP-AES.

Figure 7. Temporal potassium release profiles of poplar and corn straw sequentially treated with H<sub>2</sub>O, NH<sub>4</sub>Ac and HCl. The potassium release profiles of raw poplar and raw corn straw are also presented as a reference.

Figure 8. Release ratio of different chemical forms of potassium during the combustion of poplar and corn straw.

Figure 9. Temporal potassium release profiles of raw biomass and biomass samples with 3% additives of silica, alumina, kaolin and mica.

Figure 10. Efficiency of four additives, i.e., silica, alumina, kaolin and mica, on reducing potassium release during the combustion of poplar and corn straw.

*Color figures can be used for the online PDF version and the gray style for hardcopy reproduction.*