

1 **Enhanced coagulant extraction from *Jatropha curcas* in aqueous solutions and the**  
2 **application in turbidity removal**

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19

20 **ABSTRACT**

21 In this study, the effect of the extraction medium on the properties and efficiency of bio-  
22 coagulant, extracted of *Jatropha curcas* (Jc), in turbidity removal from aqueous solutions has  
23 been investigated. The optimised values of NaCl concentration (*i.e.* NaCl), solution pH and  
24 solution temperature were identified to improve the extraction of the coagulant. The optimised  
25 conditions were associated with an optimum coagulant dosage and a maximum turbidity removal  
26 from the synthetic aqueous solutions. The highest turbidity reduction was achieved with the  
27 coagulant extracted at a solution pH of 10 and an extraction temperature of 60 °C (pH10/60°C-

28 JcPc). Under these conditions, the coagulant dosage required was reduced by 80-90%, depending  
29 on the coagulation pH. At the coagulation pH=6, the pH10/60°C-JcPc well reduced the turbidity  
30 by 85%. However, the distilled water-based extract failed to lower the turbidity. Several  
31 analytical techniques were employed to characterize the nature of the active components derived  
32 from Jc. SDS-PAGE electrophoresis showed that Jc extract was mainly made up of proteins with  
33 molecular weights between 20 and 35 kDa. The optimized extraction conditions significantly  
34 improved the efficiency of this promising bio-derived coagulant in turbidity reduction. This  
35 study demonstrates the potential employability of these enhanced bio-coagulants. This can be a  
36 step ahead in helping with the development of sustainable processes in (waste)water treatment,  
37 particularly in tropical regions *e.g.* Malaysia with an abundant access to Jc.

38

39 Keywords: *Jatropha curcas*; natural coagulant; water treatment; biomass; protein; turbidity  
40 removal.

41

## 42 **1. Introduction**

43 Today, one of the key changes in the process industries is waste minimisation in the  
44 conversion of waste to value-added end products. Furthermore, the continual depletion of  
45 available resources has led to a rising growth in research opportunities *e.g.* the use of waste  
46 biomass in energy production and water/wastewater treatments. Natural materials are known to  
47 be effective coagulants. They are of great importance especially in countries where access to  
48 conventional chemicals has proven to be difficult or not economical [1, 2]. These easily-  
49 biodegradable biomaterials are readily found in abundance as waste by-products with practically  
50 little or no secondary large-scale application [3, 4].

51 Active components derived from natural coagulant can be produced or extracted from  
52 microorganisms, animals [5] and/or plants [6]. Plant-based coagulants are categorised into three  
53 main groups depending on the nature of their active components. The first group comprises  
54 oilseeds of which press-cake has shown a good coagulation activity with protein as their active  
55 component. The next group is mucilage of the cactus family plants with a mixture of  
56 polysaccharides, capable of treating water *via* floc forming. And finally, tannin, a general name  
57 given to large polyphenolic compounds derived from natural materials [6].

58 Among plant-based coagulants, the active component in *Moringa oleifera* (*M. oleifera*) seeds  
59 is a promising alternative for the conventional coagulants. The corresponding coagulation  
60 mechanism has been thoroughly investigated in the literature [7, 8]. It was shown that the active  
61 components in the water extract are the dimeric cationic polypeptides (6–17 kDa) with 10–11  
62 isoelectric points [9]. Another potential source of bio-coagulant is *Jatropha curcas* (Jc),  
63 sometimes referred to as the “physic nut”. The seeds are made up of about 30–35% oil. Jc has  
64 been widely grown for oil extraction from its seeds [9-11]. A solid waste residue, called press  
65 cake (Pc), with a good protein content is generated after the oil extraction process [10-12].

66 In comparison to *M. oleifera*, it has been reported [13] that the aqueous extracts of Jc kernel  
67 demonstrate an acceptable coagulation activity when tested on river water samples. The active  
68 coagulant component in the Jc is believed to be a soluble protein (Jc is an oilseed with a high  
69 protein content). It has also been reported that the key factors in increasing the solubility of  
70 protein in aqueous solutions are the ionic strength, solution pH and temperature [14-16].

71 The first objective of the present work is to investigate and optimize the extraction conditions  
72 in order to reduce turbidity in aqueous solutions with a minimum dosage of bio-coagulant. This

73 study also seeks to specify and characterize the produced extract. To the best of our knowledge,  
74 the composition, nature and properties of Jc extract has not been reported elsewhere. Elemental  
75 analysis, FTIR analysis, enzymatic hydrolysis and sodium dodecyl sulphate polyacrylamide gel  
76 electrophoresis (SDS-PAGE) measurements were employed in order to characterize the active  
77 components.

## 78 **2. Materials and methods**

### 79 *2.1 Materials*

80 The Jc seeds were supplied by the Malaysian Agricultural Research and Development  
81 Institute (MARDI). The raw plant was freshly collected from Universiti Putra Malaysia's farm.  
82 Kaolin, sodium hydroxide pellets and sodium chloride were purchased from R&M Chemicals,  
83 Essex, UK. Hexane from System Co., Shah Alam, Malaysia, Alcalase from Novozymes A/S,  
84 Baegsvard, Denmark and Hydrochloric acid (HCl, 36%) from Fisher Scientific, UK were the  
85 other chemicals used in the present work.

86

### 87 *2.2 Characterisation of Jc*

88 A hexane-based solid-liquid extraction process was employed in order to prepare the Jc press  
89 cake [17]. The results from the proximate and elemental analyses (Truspec CHNS/CHNSO  
90 elemental analyzer (LECO, USA)) of the shelled Jc seeds as well as the press cake are shown in  
91 Table 1. All chemicals used in the experiments were of analytical grade and were used as  
92 received without any further purification. In addition, the functional groups in Jc and JcPc were  
93 detected on a Spectrum 100 FTIR spectrometer (Thermo Nicolet) within a spectral range of  
94 4000-400  $\text{cm}^{-1}$ . The spectra of the kernel and the press cake were similarly recorded.

95

96 2.3 *Extraction of the coagulant's active component*

97 In order to extract the active component, two grams of the sieved JcPc (100-550  $\mu\text{m}$ ) was  
98 mixed with 100 ml of the extraction solution. In order to determine the optimum extraction  
99 conditions, the effects of three experimental parameters *i.e.* solution temperature, NaCl  
100 concentration and solution pH (*i.e.* the extraction pH), were studied. To achieve this, different  
101 aqueous media were used: distilled water (Favorit Water Still W4L) at neutral pH (*i.e.* pH 7) as  
102 well as at pH values of 9 and 10 (adjusted by using 0.1 and 1 M NaOH) and NaCl solutions (0.1,  
103 0.2, 0.3, 0.5, 1.0, 2.0 M) [11, 18]. The extraction temperature was studied at three levels: the  
104 room temperature (RT), 40 °C and 60 °C [10]. All mixtures were continuously stirred for five  
105 minutes on a heated hotplate, using a magnetic stirrer (Fisher Scientific Isotemp). The  
106 suspension was next filtered through a muslin cloth and cooled down to room temperature. The  
107 supernatant was then centrifuged (High Speed Refrigerated Centrifuge CUBOTA 6500) at 3000  
108 rpm for 15 minutes. These coagulant solutions, extracted in distilled water (DW) and NaCl  
109 solutions, were referred to as DWE-JcPc and SCE-JcPc (*i.e.* Distilled Water Extract/Sodium  
110 Chloride Extract of JcPc), respectively. A fresh solution was prepared for each sequence of  
111 experiments to prevent any change in coagulation activity due to microbial decomposition of the  
112 organic compounds during storage. The coagulant extract from JcPc at optimum extraction  
113 condition was labelled as pH10/60°C-JcPc indicating that the extraction solution pH and solution  
114 temperature were adjusted at 10 and 60 °C, respectively.

115

116 2.4 *Isolation, partial purification and characterization of the active component*

117 In order to identify the nature of the active components in Jc, enzymatic hydrolysis was  
118 performed by adding Alcalase to pH10/60°C-JcPc. The solution pH of the pH10/60°C-JcPc was  
119 adjusted at 8 using HCl (0.1 M and 1 M) prior to the addition of the enzyme (pre-adjusted  
120 medium pH). The mixture was then continually stirred inside a water bath regulated at 50 °C for  
121 6 hr [19, 20]. During this process, the entire peptide bonds were broken down [21]. This would  
122 then allow a coagulation test to potentially prove the quality of the extracted active component in  
123 the solution [19].

124 In order to study the nature of the active component, three samples from the original  
125 pH10/60°C-JcPc solution (30 ml, pH=8) were prepared in three volumetric flasks (100 ml).  
126 Alcalase (500 µl) was next added to one of the three samples. The second sample was used as the  
127 control experiment with no added Alcalase. Finally, the third sample (Alcalase free) was placed  
128 and kept inside the refrigerator (4-7 °C) in order to prevent any microbial decomposition of the  
129 organic compounds. An enzyme control test was also employed by adding of Alcalase (500 µl)  
130 to distilled water (30 ml, pH = 8). After the completion of the hydrolysis reactions, the  
131 coagulation activities of all four samples were tested *via* the jar test.

132 Active proteins were isolated and characterized using a range of techniques including  
133 isoelectric precipitation, dialysis and electrophoresis. A modified version of an existing method  
134 [10] was employed in order to precipitate the active proteins from the JcPc solutions. In order to  
135 isolate the protein from the pH10/60°C-JcPc, the pH of the coagulant solution was adjusted to 5  
136 using HCl (Fisher Scientific 36%) before being centrifuged at 3000 rpm for 20 min at room  
137 temperature (High Speed Refrigerated Centrifuge CUBOTA 6500). The generated white

138 suspension was then dissolved in distilled water and was continually stirred for four hours on a  
139 magnetic hotplate (Fisher Scientific Isotemp). Finally, the non-soluble residue was filtered firstly  
140 through a Whatman No. 1 filter paper and then through a 0.45 and 0.22  $\mu\text{m}$  nylon membrane.  
141 The supernatant was dialyzed overnight at 4 °C against deionized water in a dialysis bag (UC36-  
142 32-100, Viskase Sales Corp) with a molecular weight cut-off of 12-14 kDa.

143 The protein's Molecular Weight Distribution of the distilled-water extract and the purified  
144 pH10/60°C-JcPc samples were monitored by SDS-PAGE (sodium dodecyl sulphate  
145 polyacrylamide gel electrophoresis) on 12.5 % (w/v) polyacrilamid gel. Protein bands were  
146 visualized *via* Coomassie brilliant blue R-250 staining [22].

147 The total sugar and protein contents of the natural coagulant solutions were measured *via* the  
148 phenol-sulfuric acid method with glucose as the standard [23] and the Bradford method with  
149 bovine serum albumin as the standard, respectively [12].

150

### 151 2.5 *Turbid water samples*

152 In order to identify the optimised experimental condition for the extraction of the active  
153 component of Jc, synthetic kaolin turbid water was prepared and used in the subsequent turbidity  
154 removal experiments. Kaolin was used to establish a desired level of turbidity. By adding 7.5 ml  
155 of kaolin stock solution [24] to 500 ml of tap water and storing the solution over night to  
156 maintain a constant temperature and remove any residual chlorine, a 200-NTU turbid water was  
157 successfully synthesized. The turbidity was determined using a HACH Turbidimeter (Model  
158 2100 N). The pH of the turbid water samples was  $7.41 \pm 0.07$  and where indicated, the desired

159 pH (*i.e.* coagulation pH) was adjusted by adding hydrochloric acid (0.1 M and 1 M) and sodium  
160 hydroxide (0.1 M and 1 M).

## 161 2.6 Coagulation experiments

162 Jar flocc test, comprising a series of batch experiments, was employed in order to study the  
163 coagulation process. All experimental parameters were kept constant during the tests except for  
164 the target variable. The coagulation activities of the different extracts were evaluated in a jar  
165 tester (VELP, model JLT6). Samples were added to beakers filled with turbid water in different  
166 dosages (10-400 mgL<sup>-1</sup>). The solutions were then constantly stirred (100 rpm) for 4 min,  
167 followed by a slow mixing phase (40 rpm) for 25 min. After about 30 minutes of sedimentation,  
168 an aliquot of the clarified sample (20 mL) was collected from the top of the beaker and the  
169 residual turbidity was measured. The final (residual) turbidity of the treated water samples was  
170 measured and the turbidity removal percentage was calculated by the difference between the  
171 initial and the final turbidity values divided by the initial turbidity, multiplied by 100. All  
172 experiments were run at room temperature (25 ± 1 °C).

173 In order to investigate the reproducibility of the results, the extraction experiments in pH 10  
174 and temperature 60 °C were repeated in quintuples and in irregular intervals for two months  
175 followed by the subsequent analyses of the efficiency of the pH10/60°C-JcPc in turbidity  
176 removal at coagulation pH of 4. Each experiment was run in triplicates. The residual turbidity of  
177 these runs *i.e.* 4.22±0.43, 4.02±0.20, 4.63±0.34, 5.48±0.45, 4.65±0.31 NTU, indicates that the  
178 extracted natural coagulant could successfully reduce the turbidity of the synthetic turbid water  
179 with a high degree of reproducibility.



180 **3. Results and discussions**

181 *3.1 Optimisation of the extraction conditions*

182 The coagulation activity of the DWE-JcPc was investigated in a synthetic aqueous kaolin  
183 solution. Through a series of initial tests, it was concluded that acidic pH facilitates turbidity  
184 reduction from synthetic water. Fig. 1 presents the effect of DWE-JcPc dosage on residual  
185 turbidity of synthetic aqueous kaolin solution at coagulation pH values of 4, 5 and 6.

186 The residual turbidities of water treated with the optimum dose of the coagulating solution -  
187 corresponding to the highest turbidity reduction - were found to be 5 and 33 NTU at pH 4 and 5,  
188 respectively. The optimum doses of coagulant at pH 4 and 5 were 100 and 200 mgL<sup>-1</sup>,  
189 respectively. However, at a coagulation pH of 6, DWE-JcPc could not reduce the turbidity to an  
190 acceptable level (*i.e.* >30% [25]) and therefore, distilled-water extraction proved not to be  
191 suitable for successful coagulation at coagulation pH of 6.

192 The elemental analysis on the JcPc (Table 1) showed an enrichment of protein in the sample:  
193 8.38 wt% nitrogen (7.69 wt% carbon) as compared to the kernel, which contained only 4.98 wt%  
194 nitrogen (57.05 wt% carbon). The crude protein contents of Jc's kernel and JcPc are 31.52% and  
195 54.04%, respectively (Table 1). Both kernel and press cake were further analysed *via* FTIR to  
196 confirm the presence of the protein. As illustrated in Fig. 2, FTIR analysis for Jc kernel and press  
197 cake showed two strong absorption bands at 1635 cm<sup>-1</sup> and another at 1535 cm<sup>-1</sup>. Another band  
198 was also recorded in the range of 1240-1246 cm<sup>-1</sup>. These peaks are characteristic of carbonyl  
199 C=O stretching vibrations in primary, secondary, and tertiary amides, respectively [26, 27]. This  
200 suggests that the Jc seeds hold up a high percentage of protein within them. The comparison  
201 between spectra of the press cake and the kernel demonstrated that the amide infrared absorbance

202 has not been remarkably altered in the press cake due to the structural changes in protein after  
203 solvent extraction of lipids.

204 Therefore, the active component of Jc press cake as a coagulant might be protein molecules.  
205 In both laboratory and commercial-scale extraction processes, water with sodium or potassium  
206 hydroxide are used to modify the pH and to ultimately extract protein from press cake [10, 28].  
207 On this ground, the same approach was adapted throughout the JcPc active component extraction  
208 process.

209 With NaCl solution, it was observed that the optimum dosage of JcPc extract was halved  
210 compared to when water was used as the extraction medium at coagulation pH 4. The  
211 corresponding amount of SCE-JcPc was 40 mgL<sup>-1</sup>. On the other hand, the lowest concentration  
212 of NaCl showing the same degree of turbidity reduction was 0.3 M. Additionally, higher  
213 concentrations of up to 0.5 M did not show any significant difference while elevated salt  
214 concentrations (1.0 and 2.0 M NaCl) had a negative impact on turbidity reduction. The decrease  
215 in coagulation performance at 1.0 and 2.0 M could be due to the “salting-out” phenomena [10].

216 In the next phase of the experiments, the effects of temperature and pH on extraction were  
217 investigated. Although the temperature of the extraction solution was expected to improve the  
218 extraction yield (increasing temperatures facilitated the molecular dissolution of solutes in the  
219 solvents), the results indicated that solely preheating the coagulant solution would not have a  
220 significant effect on the coagulating efficiency. It has been observed that in some cases, an  
221 increase in temperature could decrease the protein solubility at isoelectric point (pI); however, at  
222 other pH values (below and above pI), the effect of temperature on solubility of protein was  
223 strongly affected by solution pH [28]. On the other hand, Saetae et al. 2011 [16] reported that Jc

224 protein solubility increases with temperatures within the range of 30 to 50 °C at an extraction pH  
225 of 12. In general, it is understood that the effect of temperature on solubility is strongly  
226 dependent on the pH of the extracting solution and therefore, there exists an interaction between  
227 these two experimental factors. Hence, in the subsequent experiments, the effects of temperature  
228 and pH of the media were studied together.

229 Fig. 3 demonstrates the effects of ionic strength, pH and temperature of the extraction solution  
230 on the optimum coagulant dosage to achieve a residual turbidity of  $5 \text{ NTU} \leq$  in synthetic water at  
231 a coagulation pH of 4.

232 The optimum dosage was observed to be 100, 40 and 20  $\text{mgL}^{-1}$  for DWE-JcPc, SCE-JcPc and  
233 pH10/60°C-JcPc at a coagulation pH of 4, respectively. A notable achievement was the  
234 improvement in coagulation activity of JcPc extract at coagulation pH values of 5 and 6 by  
235 changing the extraction pH and the temperature of the extraction media. Fig. 4 draws a  
236 comparison among various extracting solutions with respect to turbidity removal at coagulation  
237 pH values of 5 and 6. The results show that the extraction of active components at an extraction  
238 pH of 10 and higher temperature substantially improved the performance of coagulant at  
239 coagulation pH values greater than 4.

240 The efficiency of different extracting solutions at coagulation pH=4 was understood to be the  
241 same in terms of the observed residual turbidity. They all showed residual turbidity of  $\leq 5 \text{ NTU}$ .  
242 However, the optimum coagulant dosages dropped by 80% and 90% for coagulation pH 4 and 5,  
243 respectively. Additionally, a higher coagulation activity (by 91.6%) with the pH10/60°C-JcPc  
244 was observed at coagulation pH=5 comparing with 83% when using DWE-JcPc. Therefore,  
245 regarding the optimum dosage improvement, the highest achieved turbidity removal with  
246 pH10/60°C-JcPc at coagulation pH=5 was almost 11 times higher than that of distilled water

247 extract. Interestingly, at the coagulation pH=6, and with the use of an alkaline-medium extract,  
248 the coagulation activity increased by 85% despite the absence of coagulation activity with  
249 distilled water extract. Therefore, it is concluded that extraction at pH 10 and at 60 °C presents  
250 two major advantages: a reduction in the optimum dosage to achieve the maximum turbidity  
251 removal and the improvement of coagulation activity at coagulation pH=5 & 6. Although salt  
252 extraction solution showed its capability in reducing the optimum dosage at coagulation pH=4  
253 and it also indicated an improvement in coagulation activity at coagulation pH=5 compared to  
254 DWE-JcPc, it was still not as efficient as the solution extracted at pH 10 and at 60 °C.

255 Since the active coagulant component was now believed to be protein, the protein and  
256 carbohydrate content of the extractant were subsequently analysed. The results indicate a  
257 significant increase in the yield of protein extraction from JcPc through alkaline extraction.  
258 Extraction at 60 °C and a pH of 10 corresponded to a higher protein content (*i.e.*  $6.65 \pm 0.20 \text{ gL}^{-1}$   
259 <sup>1</sup>) than extraction in a water-only medium (*i.e.*  $0.81 \pm 0.06 \text{ gL}^{-1}$ ). Furthermore, the total amount  
260 of carbohydrate in DWE-JcPc and pH10/60°C-JcPc were  $1.35 \pm 0.17 \text{ gL}^{-1}$  and  $1.63 \pm 0.02 \text{ gL}^{-1}$ ,  
261 respectively. Similar findings by other researchers [10, 29] have also been reported in the  
262 literature for optimising the extraction of protein from oil seed biomass.

263

### 264 3.2 *Isolation and identification of pH10/60°C-JcPc active component*

265 In order to characterize the extracts, several characterization techniques were employed.  
266 Protein hydrolysis and SDS-PAGE electrophoresis were used to characterize the coagulation  
267 active components in Jc.

268 The hydrolysis process is a reaction in which a substance is degraded. Enzymatic hydrolysis  
269 involves minimum side reactions and leads to a limited hydrolysis of selected bonds. Proteases  
270 hydrolysis breaks down proteins into various peptides which are further reduced into amino  
271 acids. This leads to a complete degradation of protein structure [19]. The results could support  
272 our hypothesis that the active component of Jc-derived coagulant is a protein if the hydrolysed  
273 sample does not show a significant coagulation activity. Fig. 5 compares the performance of the  
274 pH10/60°C-JcPc and the hydrolysed pH10/60°C-JcPc solutions for their turbidity removal.

275 Sample no. 1, 2 and 4 were maintained inside a water bath under identical Alcalase hydrolysis  
276 conditions. The hydrolysed pH10/60°C-JcPc solution did not show any coagulation activity. The  
277 turbidity removal of the treated water using the hydrolysed pH10/60°C-JcPc was measured to be  
278 2-5% compared to the turbid water treated with sample no. 2 and 3 (*i.e.* 85-92%). This indicated  
279 that sample no. 1 completely failed to reduce the turbidity and therefore, no coagulation activity  
280 was observed. Alcalase just reacts with protein components and break downs peptide bonds,  
281 resulting in new components such as amino acids with completely different properties from  
282 proteins. In addition, the results of sample no. 4 confirmed that Alcalase did not demonstrate any  
283 coagulation activity.

284 The SDS-PAGE was used to determine the molecular weight profile for the isolated proteins.  
285 The SDS-PAGE patterns of pH10/60°C-JcPc (Fig. 6 (a)) contain three major bands indicating  
286 the presence of various types of proteins with different molecular weights. The highest protein  
287 intensities of pH10/60°C-JcPc are grouped into two classes of molecular weights: <25 kDa and  
288 >25-35 kDa. In general, a minimum number of 25 protein bands are present in the Jc seed  
289 protein [18]. The number of proteins extracted in distilled water was much larger than the  
290 optimum extraction conditions while the concentration of the target protein was significantly

291 higher in the pH10/60°C-JcPc solution. These results were consistent with the findings by  
292 Hamarneh et al. 2010 [22]. They stated that the molecular weight of the protein in the Jc extract  
293 (under isoelectric conditions) contains three major bands between 20 and 45 kDa (Fig. 6 (b)). In  
294 our study, this was between 20 and 35 kDa.

295 The total protein content in pH10/60°C-JcPc after isoelectric precipitation was measured to be  
296  $1.5 \pm 0.06 \text{ gL}^{-1}$ . However, the total amount of carbohydrate was observed to be negligible. This  
297 also confirmed that the protein isolation procedure was successful. The protein content of the  
298 pH10/60°C-JcPc after isoelectric precipitation was 77% less than of the pH10/60°C-JcPc, owing  
299 to the loss of proteins during the precipitation and dissolution stages.

300

#### 301 **4. Conclusion**

302 The purpose of this study was to optimise the extraction method of the active coagulation  
303 component from Jc seeds. In order to identify the extracted species, a range of characterisation  
304 techniques were employed. The key findings in this study are summarised as follows:

305 1- Among various extraction media employed to extract the active components, an extraction  
306 medium with a pH of 10 and a temperature of 60 °C was found to be the optimised condition for  
307 both maximum turbidity removal and optimum coagulant dosage required. In the removal of  
308 kaolinite turbidity at the coagulation pH 4 and 5, JcPc extracted in an alkaline media  
309 demonstrated an improved coagulation activity with a five- and tenfold reductions in the required  
310 coagulant dosage compared to JcPc extracted in distilled water, respectively. The experimental  
311 results indicate the efficiency of the optimized extraction conditions in the active component  
312 extraction from JcPc. The protein content of pH10/60°C-JcPc was 8.2 times higher than that of  
313 the DWE-JcPc. The pH10/60°C-JcPc could efficiently coagulate more than 91% of the initial

314 200-NTU kaolin turbidity using only a dosage of 20 mgL<sup>-1</sup> at a coagulation pH of 5. However,  
315 200 mgL<sup>-1</sup> of the DWE-JcPc was required to remove only 80% of the same kaolin water. With an  
316 alkaline solution as the extractant, a coagulation activity at pH 6 corresponding to more than  
317 85% turbidity removal was observed. However, distilled water extract did not show any  
318 coagulation activity at this pH.

319 2- As confirmed *via* the elemental/proximate analyses as well as the FTIR spectra, the  
320 effective coagulant components were protein molecules. This was further confirmed through  
321 enzymatic hydrolysis. The water-extract solution demonstrated at least 20 protein bands in SDS-  
322 PAGE gel. Comparing the two SDS-PAGE gels, it was realised that the active proteins had a  
323 molecular weight between 20 and 35 kDa.

324

325 This study has showed that the pH10/60°C-JcPc can be a promising coagulant to be used in  
326 water treatment plants, especially in tropical countries such as Malaysia with an easy access to  
327 Jc. It was realized that the Jc seeds could be used as an efficient coagulant in water and  
328 wastewater treatment upon an initial purification of the active component. It is mentionable that  
329 the ultimate application of this coagulant in pilot and full-scale plants requires appropriate cost-  
330 benefit and a full techno-economic analyses for a viable commercial application of pH10/60°C-  
331 JcPc. Therefore, the authors would see it critical and with key benefits to perform such  
332 calculations in future works.

333

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- 416

417 **Table 1.** Elemental and proximate analyses of shelled Jc seed.

<b>Elemental analysis (dry wt%)</b>						
	Nitrogen	Hydrogen	Carbon	Sulfur	Oxygen	
Kernel	4.98±0.03	8.87±0.17	57.05±0.24	2.20±0.06	22.56±0.16	
Press cake	8.38±0.30	6.80±0.12	47.69±0.15	0.18±0.02	33.11±0.23	

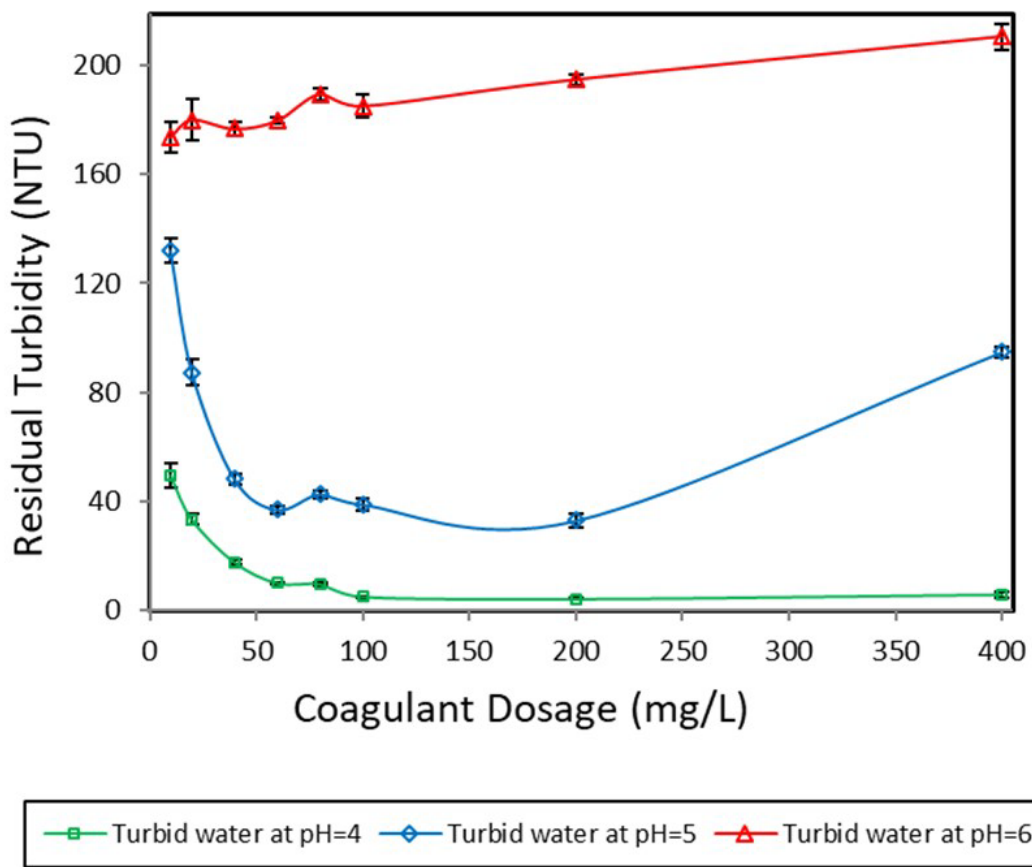
<b>Proximate analysis (raw wt%)</b>						
	Crude protein	Crude Lipids	Ash Content	Moisture Content	Crude Fiber	Total Carbohydrates*
Kernel	31.52±0.35	51.79±0.09	3.30±0.14	3.95±0.04	6.56±0.27	2.88±0.06
Press cake	54.04±0.43	16.19±0.02	6.03±0.03	5.20±0.02	7.64±0.13	10.90±0.12

418 \* Calculated from difference

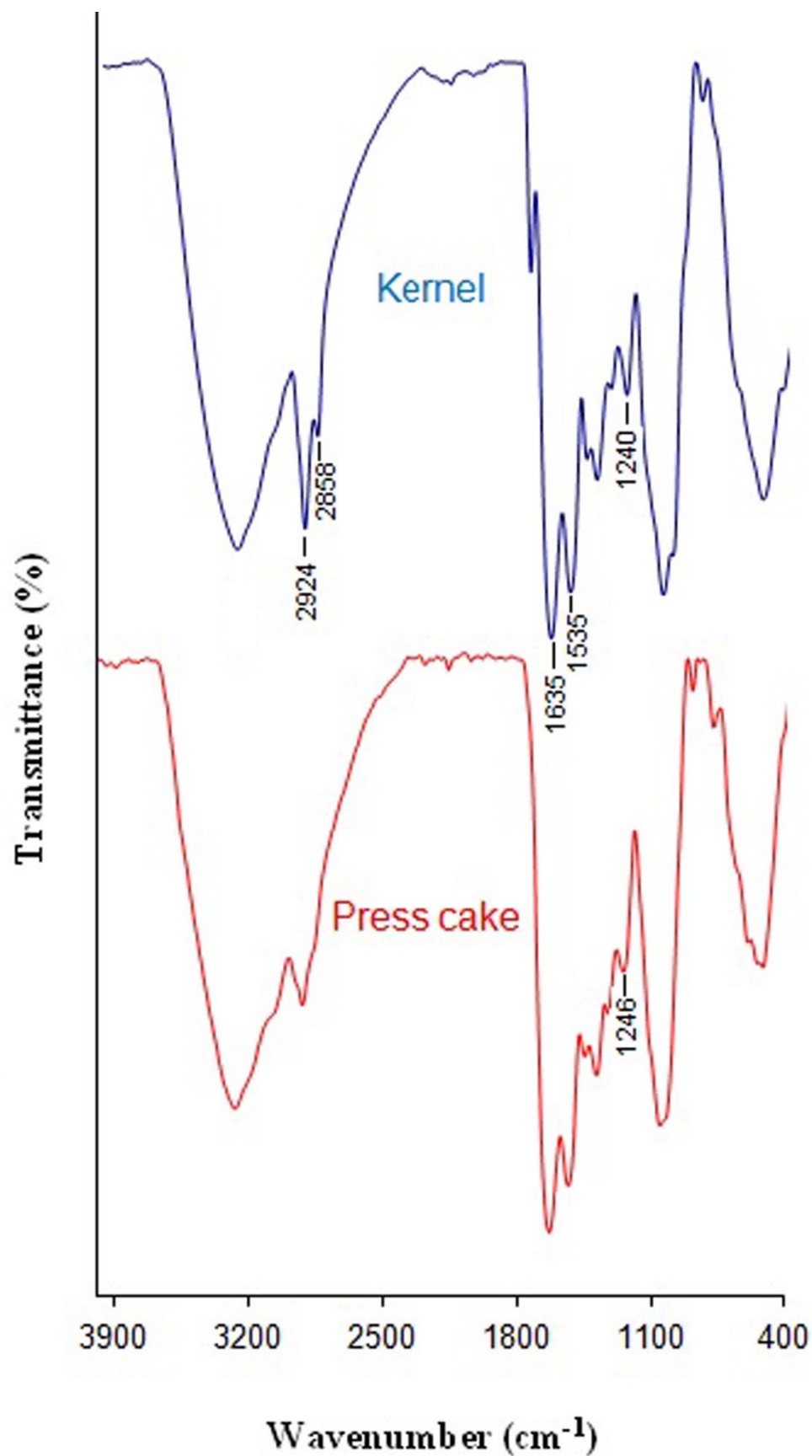
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420 **Figure captions**

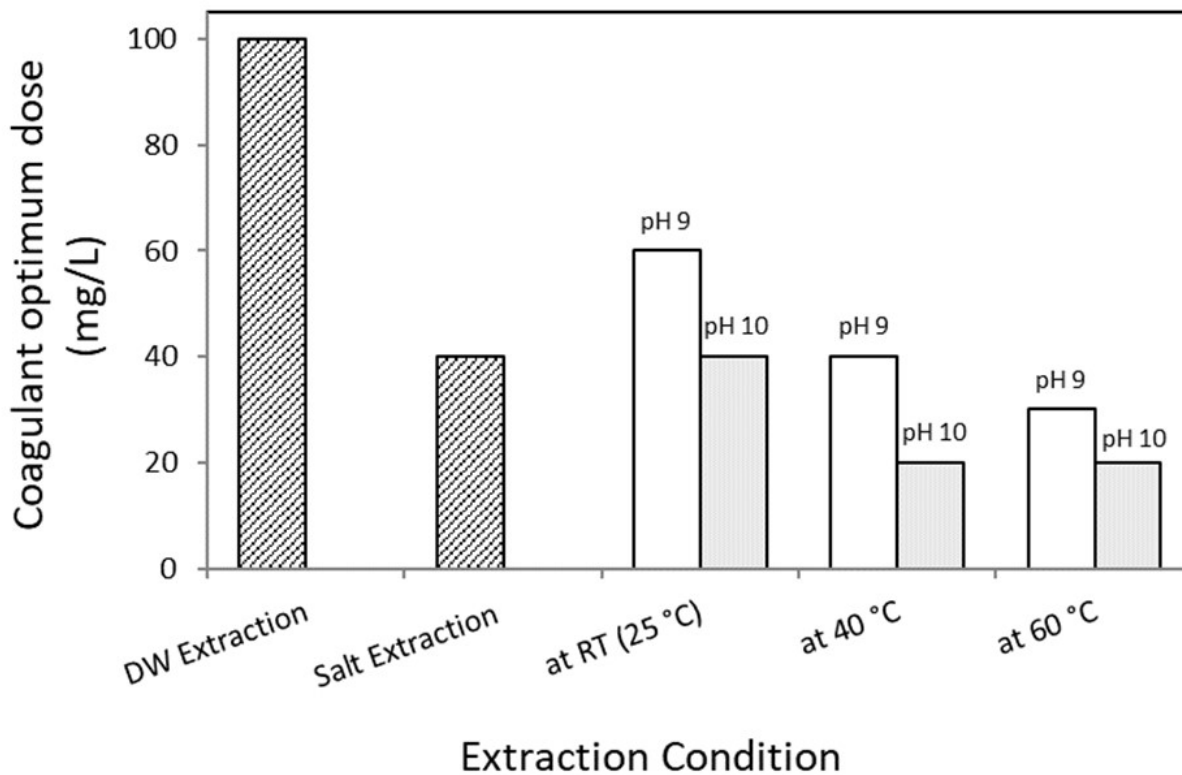
421 **Fig. 1.** Effect of water-extracted coagulant (DWE-JcPc) dosage on turbidity reduction of  
422 synthetic kaolin/water at coagulation pH values of 4, 5 and 6.



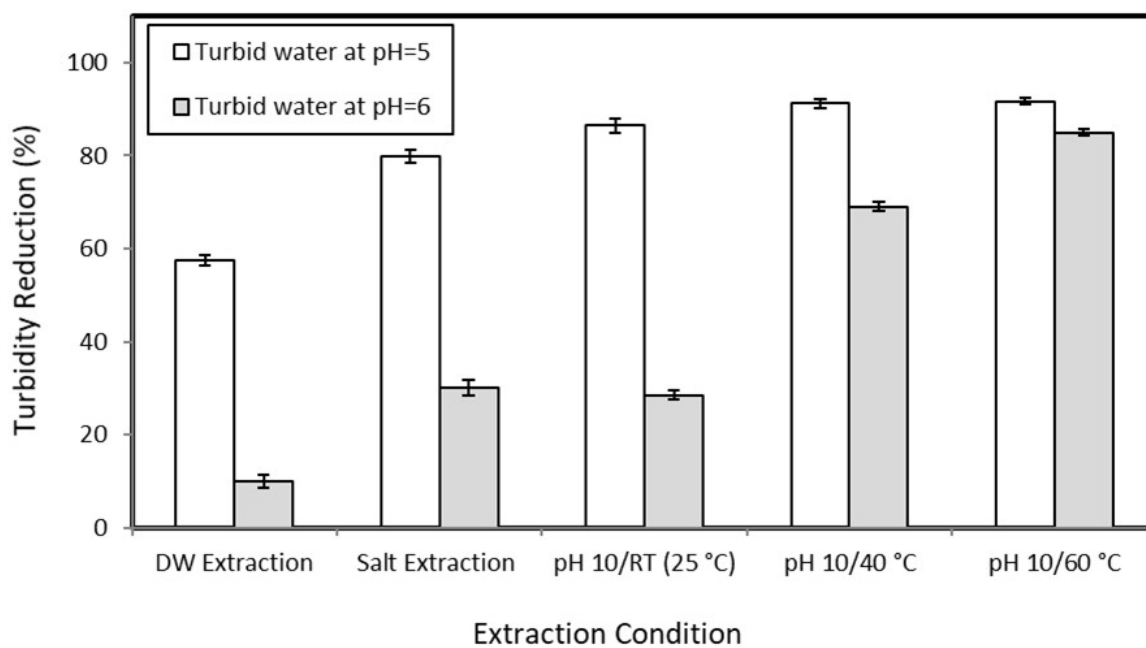
423  
424 **Fig. 2.** FTIR spectra of Jc kernel and press cake.  
425 The classical bands at 2924 and 2858 $\text{cm}^{-1}$  are typical features of compounds containing long  
426 alkyl chains [10]. The absence of 2858  $\text{cm}^{-1}$  band in the press cake spectrum validates the fat  
427 extraction from the Jc.



429 **Fig. 3.** Optimum dose corresponding to a residual turbidity of  $5 \text{ NTU} \leq$  of water at coagulation  
430 pH 4 using various extracting solutions.



431  
432 **Fig. 4.** Turbidity reduction of synthetic water at two coagulation pH values of 5 and 6 with  
433 various extracting solutions with a constant coagulant solution dosage of  $20 \text{ mgL}^{-1}$ .

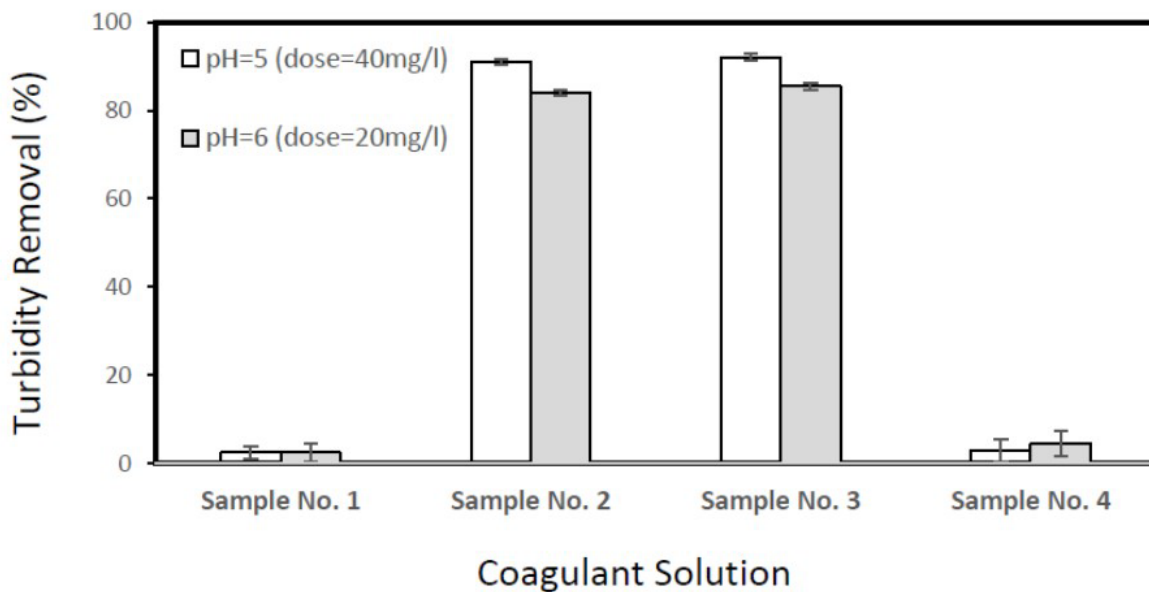


434

435 **Fig. 5.** Residual turbidity of kaolin water at two-coagulation pH values of 5 and 6 by using

436 pH10/60°C-JcPc solution under protein hydrolysis reaction.

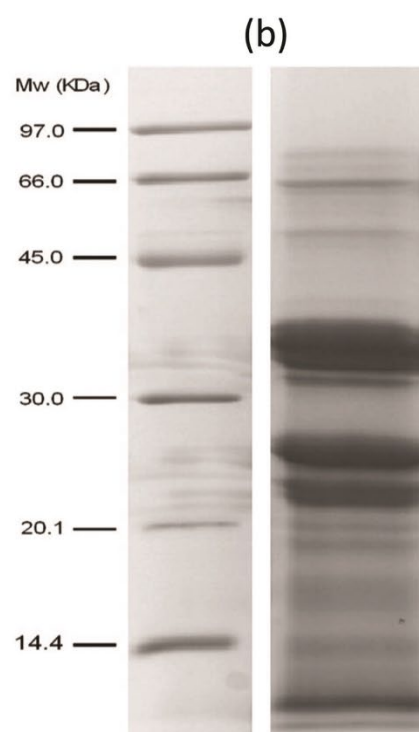
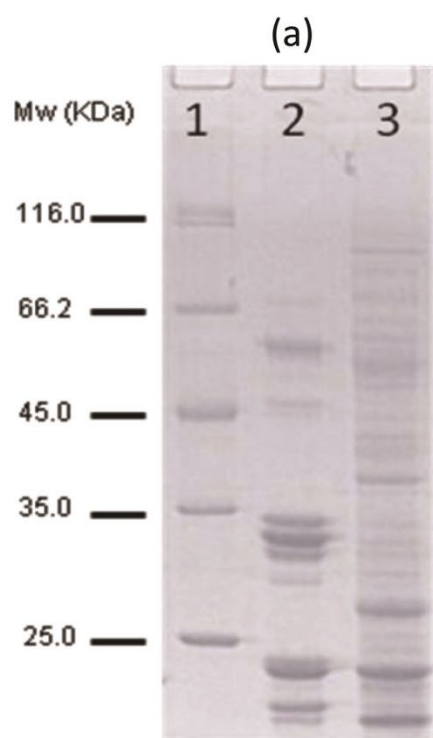




Sample:  
 No. 1: pH10/60°C-JcPc+Enzyme                      No. 2: pH10/60°C-JcPc inside water bath  
 No. 3: pH10/60°C-JcPc inside refrigerator      No. 4: Distilled water +Enzyme

437

438 **Fig. 6.** Protein molecular weight distributions of JcPc extracts: (a) Isolated protein from  
 439 pH10/60°C-JcPc by isoelectric precipitation & dialysis (2), DWE-JcPc (3), and protein marker  
 440 (1) and (b) Jc proteins extracted by isoelectric precipitation [22].



441